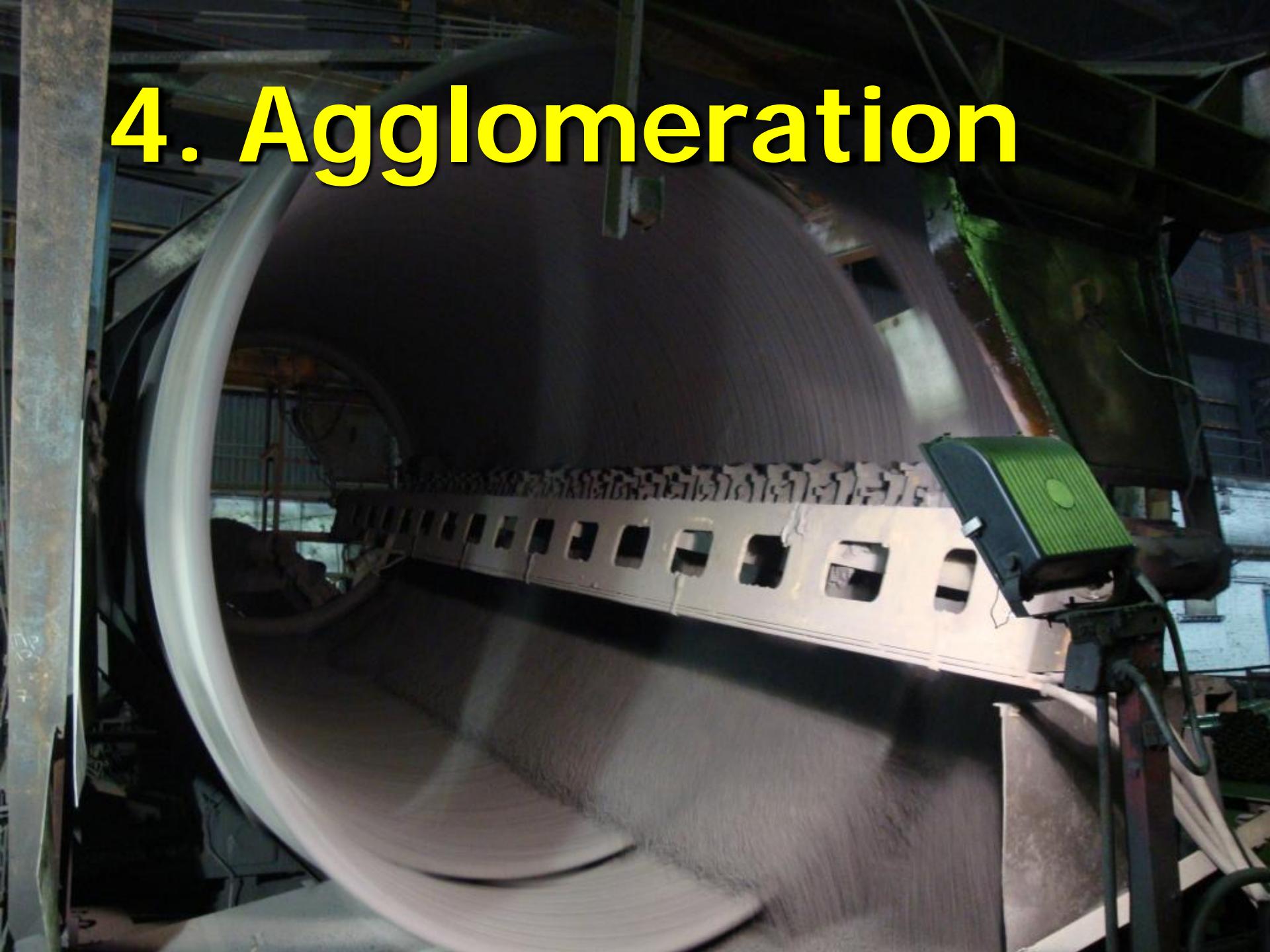


# 4. Agglomeration



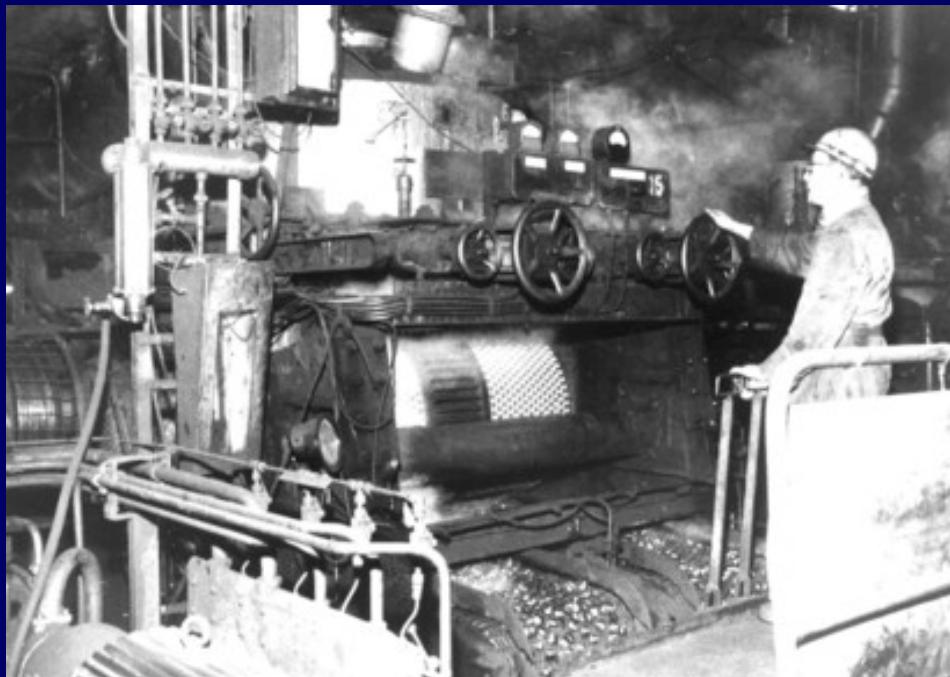
# Contents

1. Introduction
2. Briquetting
3. Sintering & nodulizing
4. Pelletizing

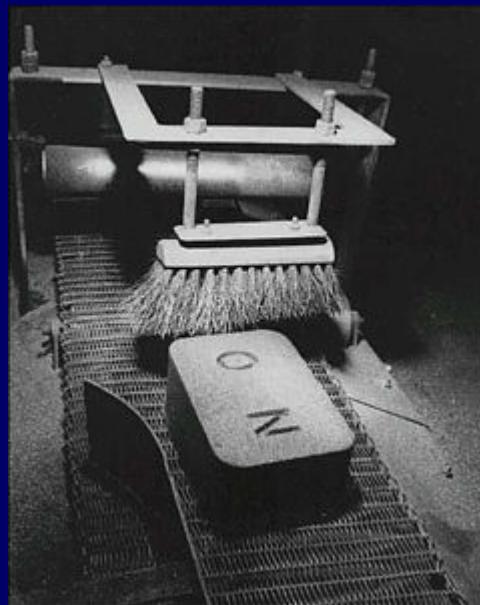
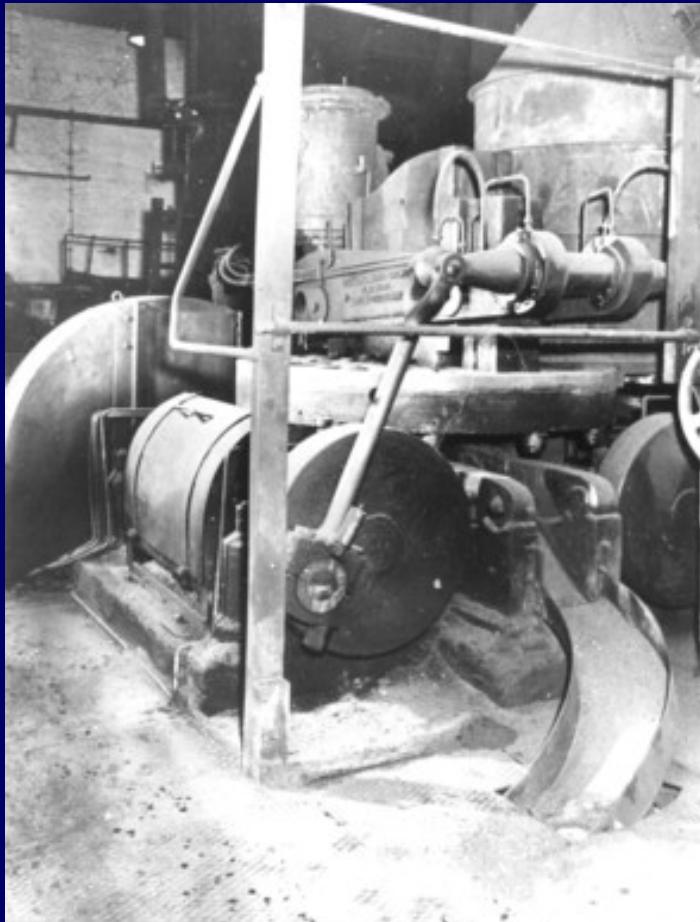
# 1. What is agglomeration ?

- Making uniform shapes from fine, incoherent particles
- Examples:
  - Coal briquettes
  - Briquettes from scrap metal turnings
  - Iron ore pellets
  - Iron ore sinter
  - Cement nodules
- Objectives:
  - Better transport and storage
  - Avoid dust
  - Better properties end use (e.g. porosity of ore bed)
  - Immobilization of certain components
  - Including components/elements (mill scale/fluxes)

# Coal briquettes (1925 – 1975)



# Block briquettes “Oranje Nassau”



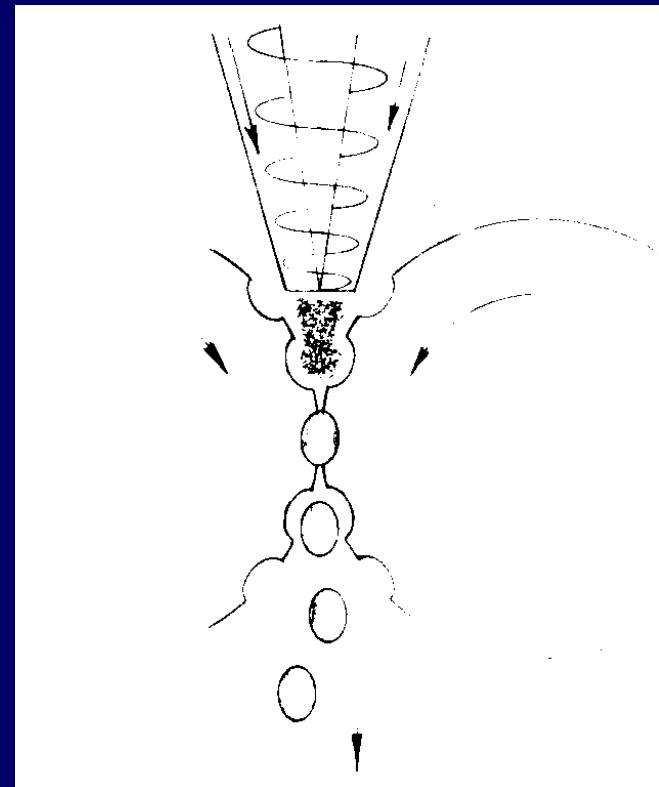
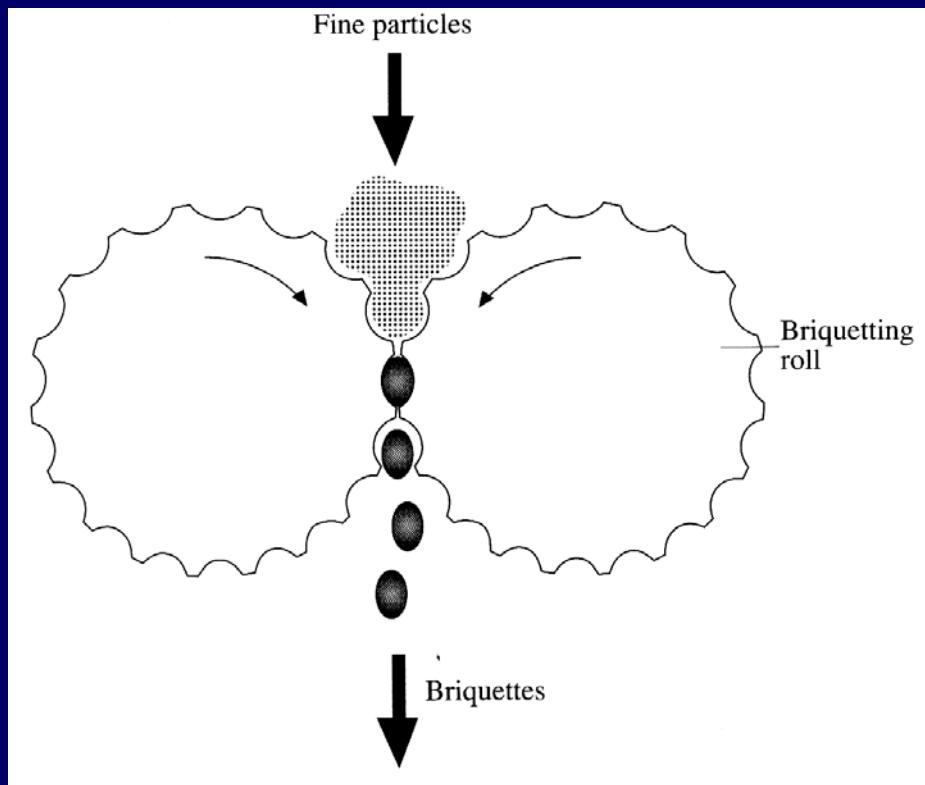
## 2. Briquetting

- Most common agglomeration method
- Applications
  - Coal
  - Coke
  - Charcoal (BBQ!)
  - Quicklime
  - Phosphate ore
  - Iron ore
  - Mill scale
  - Refuse derived fuel (RDF)
  - Flue dust
  - Sponge metals
  - Turnings
  - Salt
  - Animal food
  - Washing powder
  - ... ....



# Roll briquetting

- Geometrically shaped pieces
- Gravity fed, screw fed



# Ring roll press

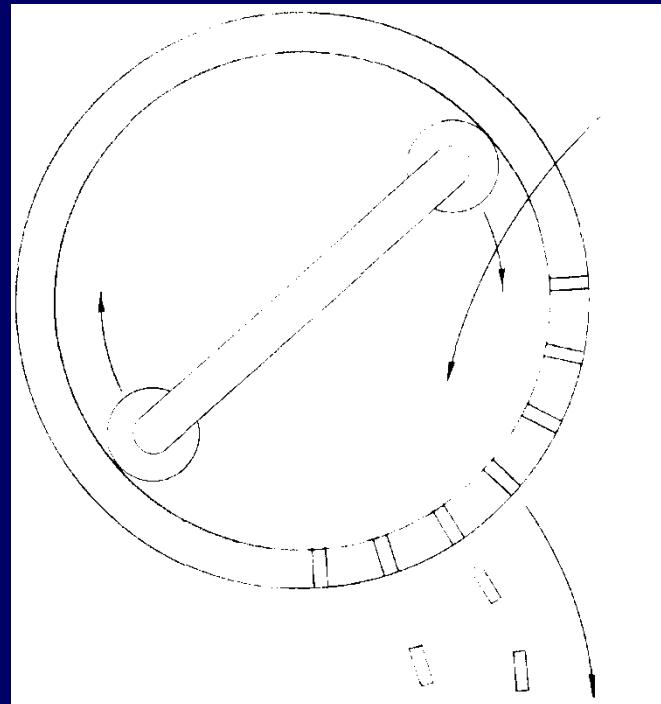


# Compaction

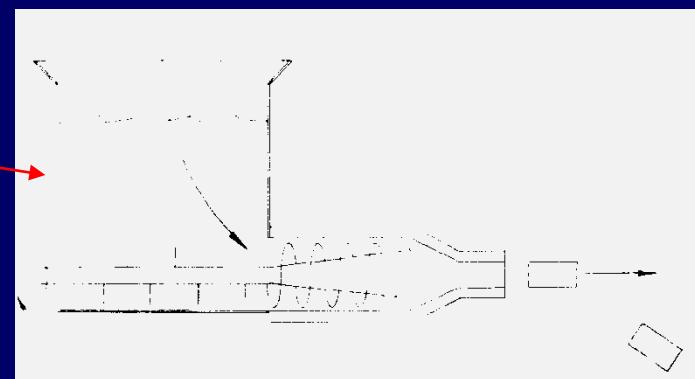
- Flakes or sheets from compressed fines
- Flakes are broken to desired size
- Fragments are larger as the input material

# Extrusion

- Forcing presses solids through a cylindrical die
- Typically 10 mm diameter,  
10 – 20 mm length

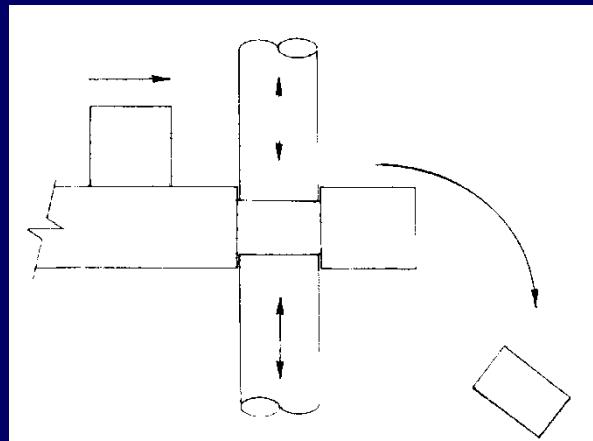


- Larger sizes made by a single press



# Tabletting

- Complex machines
- Chemical and pharmaceutical industry



# Briquetting mechanisms

- Feed must be free flowing
- Add lubricants (0.5% – 2%)
  - Water, stearic acid, Ca, Mg stearate, parrafin waxes, mineral oil, starch, graphite,  $\text{MgS}_2$
- Binders
  - Adhesive
  - Surface tension
  - Hardening binders (briquettes develop strength after pressing)

# Binderless briquetting

- Higher pressures
- Solids “welding”
- Example: salt, metal turnings
- Metal turnings should be:
  - Clean, no oil on it
  - Not weathered (no oxidized surfaces)

# Roll press action

- Exact pressure cannot be measured. Estimation:
  - Roll force / Projected area of 1 row of briquettes
  - Shear stresses cause close packing
- 
- Angle of nip: see discussion on roll mill
  - Roll spread 1.5 – 10 mm, fluctuates during operation
  - Clean discharge:
    - Pockets not too deep
    - Not too much binder
    - Pressure not too high or low

# Briquette machine performance

- Power:
  - Mixing (where binders and/or lubricants are used): 1.5 to 7.5 kW/t feed
  - Feeding: 0.4 to 4 kW/t feed
  - Briquetting: 1.5 to 20 kW/t feed
- Roll life 400 – 30.000 hours depending on abrasiveness
- Capacity Q in kg/min:  $Q = \pi DWTN\rho$

# Briquette machine performance

- Power:
  - Mixing (where binders and/or lubricants are used): 1.5 to 7.5 kW/t feed
  - Feeding: 0.4 to 1.1 kW/t feed
  - Briquetting: 1.5 to 10 kW/t feed
- Roll life 400 hours depending on diameter and abrasiveness
- Capacity Q in kg/min:  $Q = \pi DWTN\rho$

# Briquette machine performance

- Power:
  - Mixing (where binders and/or lubricants are used): 1.5 to 7.5 kW/t feed
  - Feeding: 0.4 to 1.1 kW/t feed
  - Briquetting: 1.5 to 10 kW/t feed
- Roll life 400 hours depends on roll diameter and abrasiveness
- Capacity Q in kg/min:  $Q = \pi DWTN\rho$

# Briquette machine performance

- Power:
  - Mixing (where binders and/or lubricants are used): 1.5 to 7.5 kW/t feed
  - Feeding: 0.4 to 1.1 kW/t feed
  - Briquetting: 0.5 to 1.5 kW/t feed
- Roll life 40 hours depends on roll diameter and abrasiveness
- Capacity Q in kg/min:  $Q = \pi DWTN\rho$

# Briquette machine performance

- Power:
  - Mixing (where binders and/or lubricants are used): 1.5 to 7.5 kW/t feed
  - Feeding: 0.4 to 1.1 kW/t feed
  - Briquetting: 0.5 to 1.5 kW/t feed
- Roll life 40 hours depends on roll diameter and abrasiveness
- Capacity Q in kg/min:  $Q = \pi DWTn\rho$

Roll diameter  
hours depend on  
abrasiveness

Rotation speed /min

Roll width

Briquette thickness

# Briquette machine performance

- Power:
  - Mixing (where binders and/or lubricants are used): 1.5 to 7.5 kW/t feed
  - Feeding: 0.4 to 1.1 kW/t feed
  - Briquetting: 0.4 to 1.1 kW/t feed
- Roll life 40 hours depends on  
diameter and abrasiveness
- Capacity Q in kg/min:  $Q = \pi DWTN\rho$

Roll diameter  
width  
Briquette thickness  
Density

# Performance example

Roll diameter (mm)	Effective roll width (mm)	Maximum force between rolls (tons)	Appr. Capacity* (t/hr)
130	50	10	0.15
305	76	25	1.2
380	102	50	2.5
457	152	100	5.5
610	203	150	12.5

\*For salt, with briquette density of 2165 kg/m<sup>3</sup>, roll speed is 25 rpm, and D/T = 60.

# Briquetting processes

- Low pressure (< 1 t/cm<sup>3</sup>)
  - Earthy ore, oil shale, laterite, coal/pitch, clayey bauxite, phosphate
  - 1 to 5 kWh/t
- Medium pressure (1 to 4 t/cm<sup>3</sup>)
  - 5 to 15 kWh/t
  - Salts, Calcium, magnesium oxides
- High pressure (> 4 t/cm<sup>3</sup>)
  - 15 to 30 kWh/t
  - Metal turnings, powders, sponge, steel mill dust
  - Temperature up to 1000 °C

### 3. Partial fusion

- Sintering
  - Iron ore
  - Base metal ore
- Straight grate sinter machine
- Nodulizing
  - Cement clinker, waste dusts and sludges
  - Rotary kiln

# Straight grade sinter machine



# Introduction

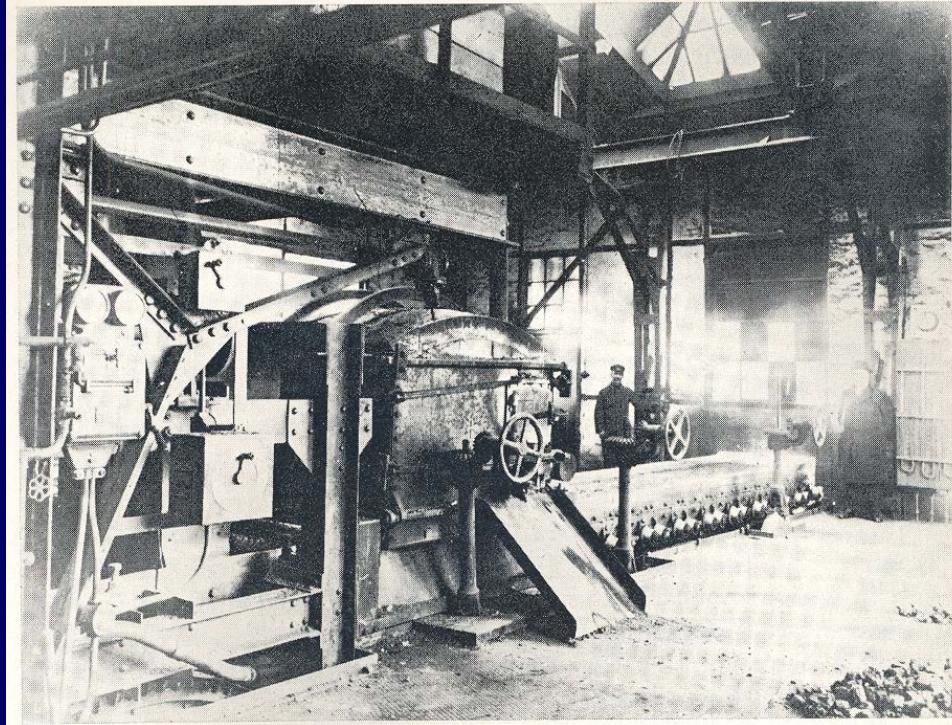
Purposes of iron ore sintering = Preparation of 'möller' for the BF

- Prepare the ore fines
- Change particle size (distribution)
- Improve reducibility
- Prevent disintegration
- Prevent LOI
- Dose fluxes
- Use of in plant revert
- Less materials to the BF



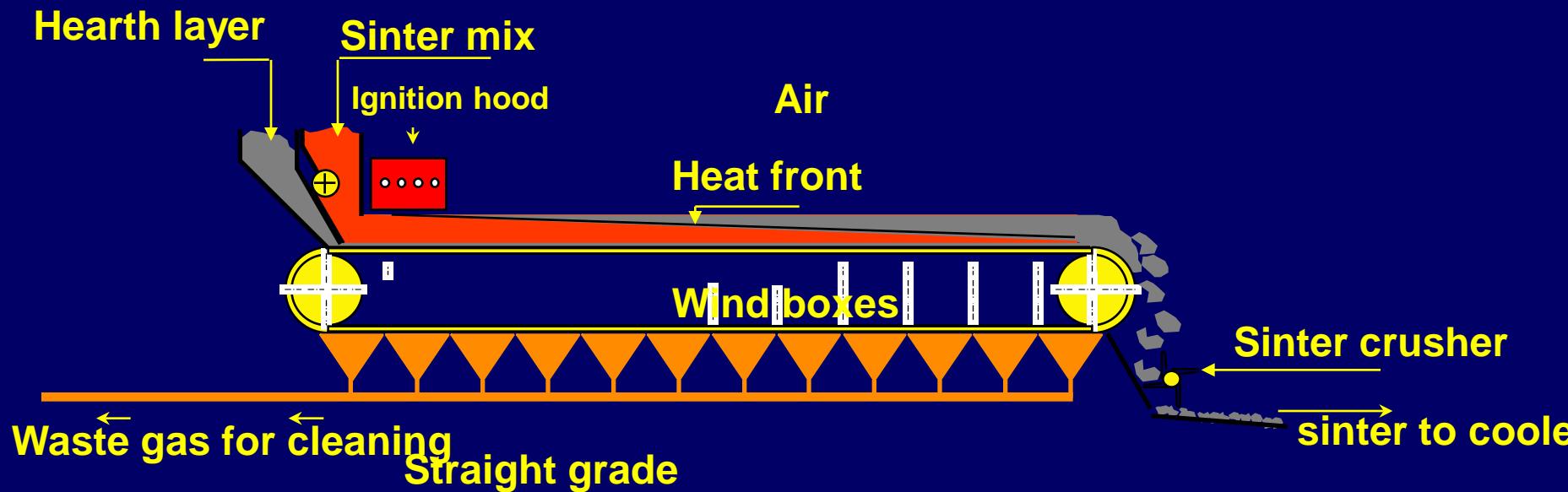
# Sintering is old technology

First principle	1897
First industrial application	1911
‘Large scale’ (75 m <sup>2</sup> )	’30
IJmuiden sinter strands	’56/’60/’63

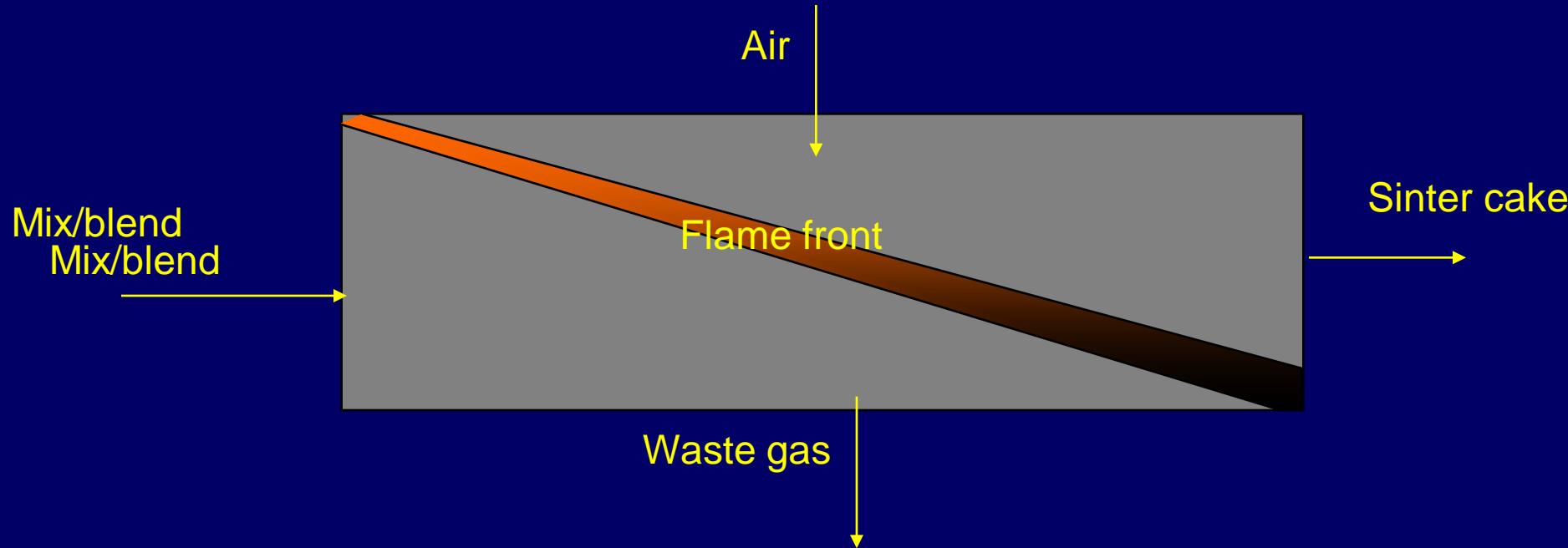


Dwight-Lloyd sinter machine 1914

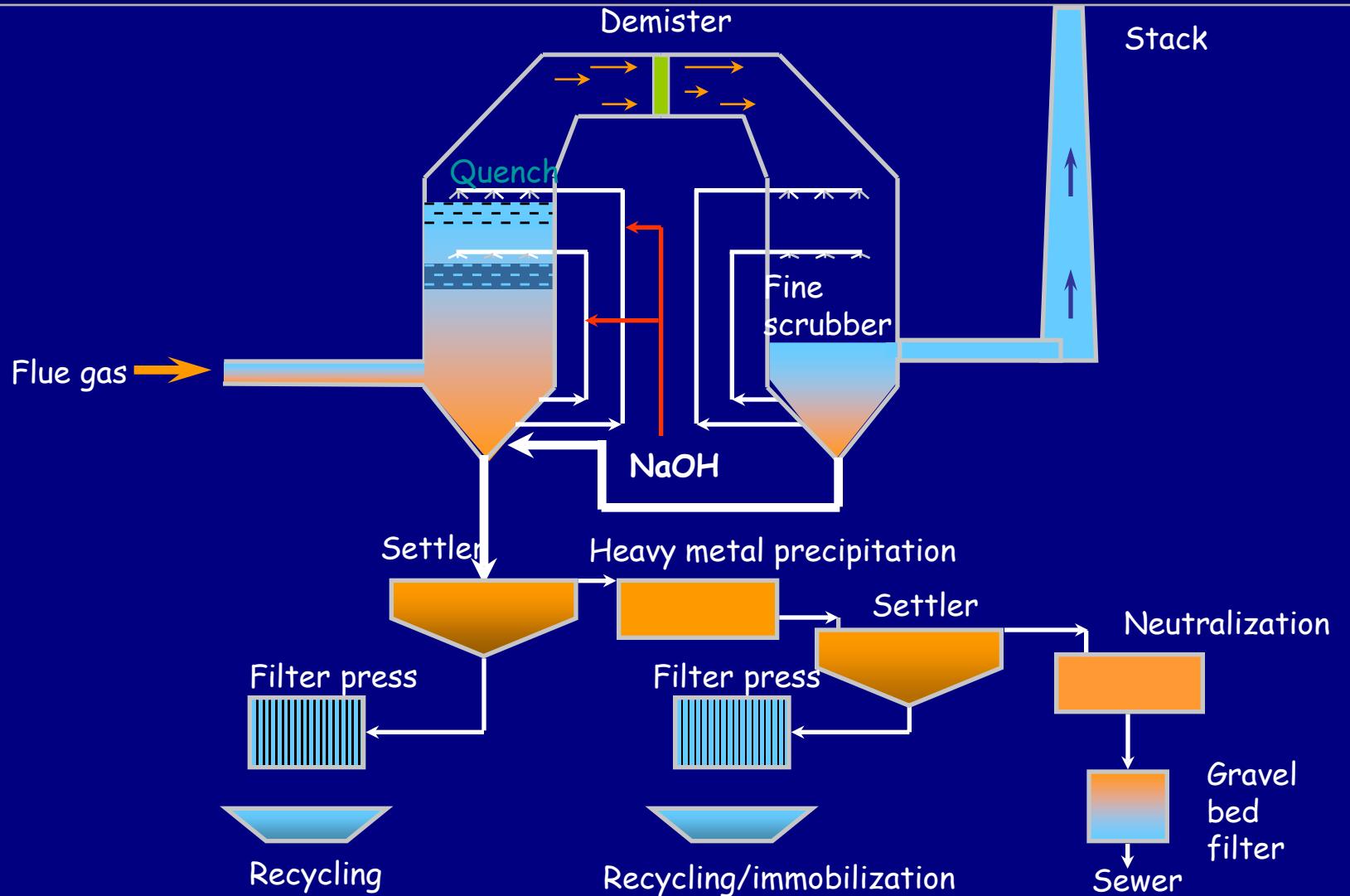
# Sinter machine



# Sintering principle



# Do not forget the environment! Gas cleaning at Corus IJmuiden



## 4. Pelletizing

- 230 Mtpa (1976) increased to 400 Mtpa (2009 est)
- Fine ground, damp, ore is rolled into 'green' balls and heat hardened

Add value to the abundant fines ores and concentrates by agglomeration at location into an agglomerate transportable to integrated steel works



# Transport



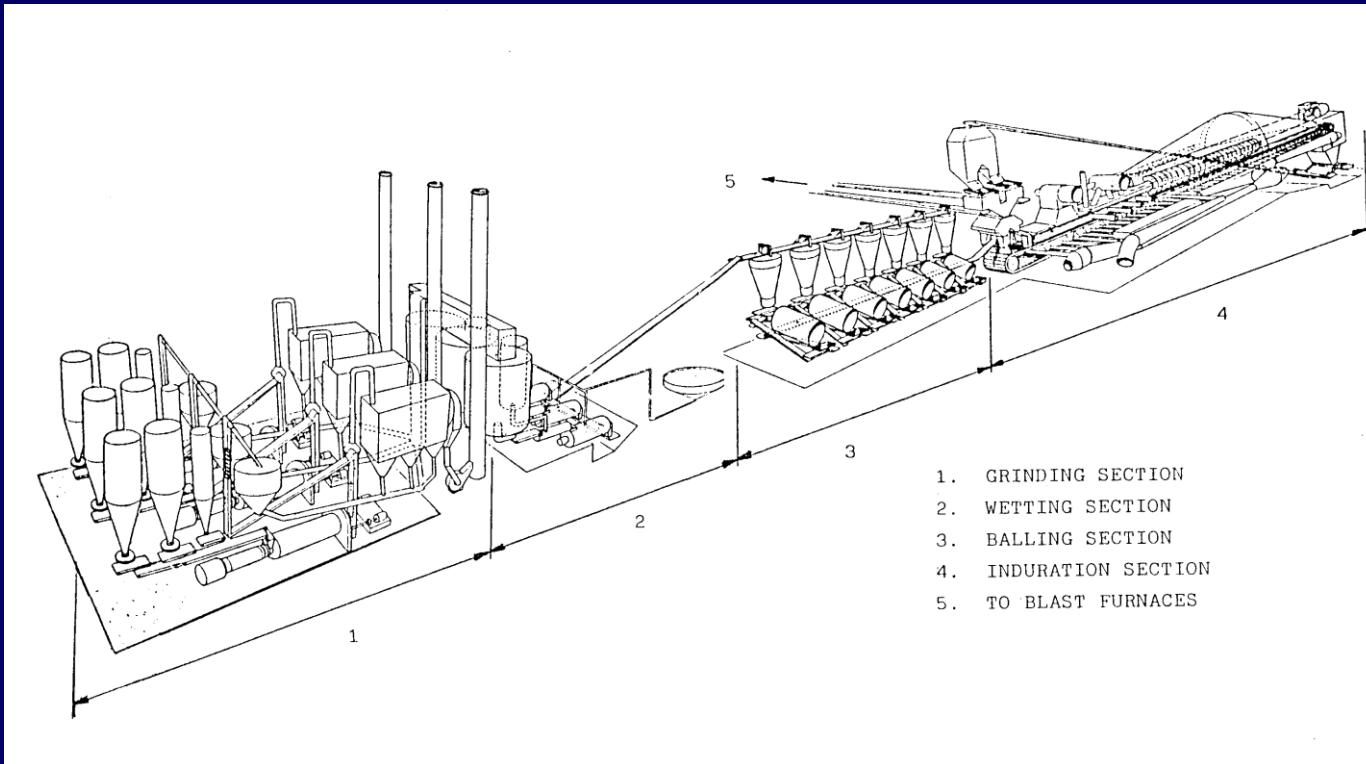
# Introduction

Technology developed in Sweden, Germany and USA

- First patent 1913
- First pilot plant 1930
- First shaft furnace 1943
- First Travelling Grate 1950's
- IJmuiden pellet plant 1970

# Corus Strip Products IJmuiden

## Pellet Plant



- Lurgi straight grate, suction surface area  $\pm 430 \text{ m}^2$
- Maximum pellet production: 5 Mtpa
- Flue gas scrubbers with water treatment plant

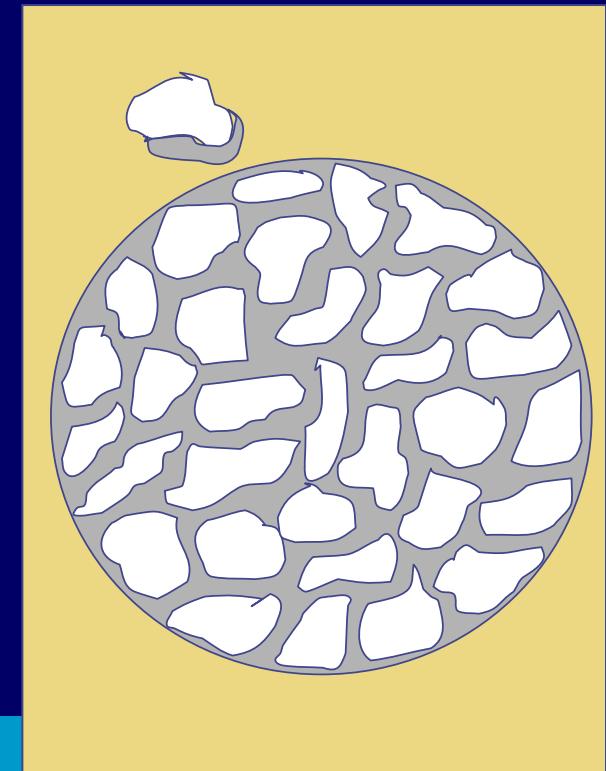
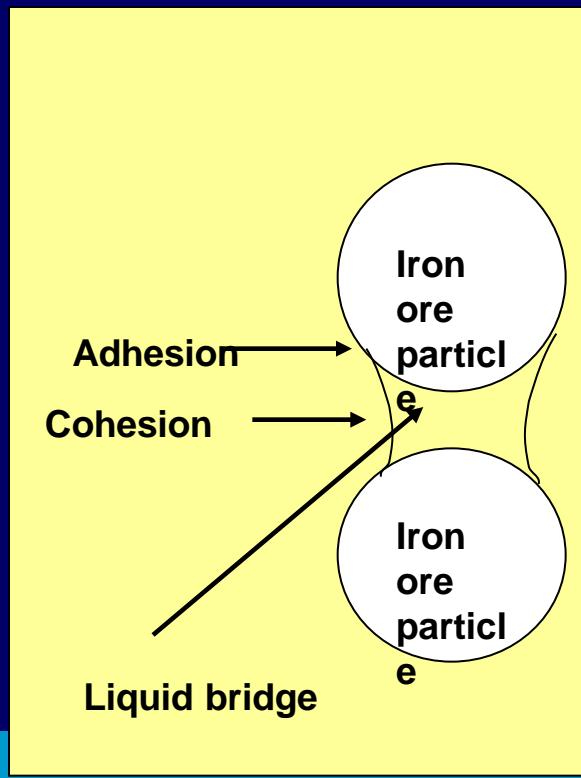
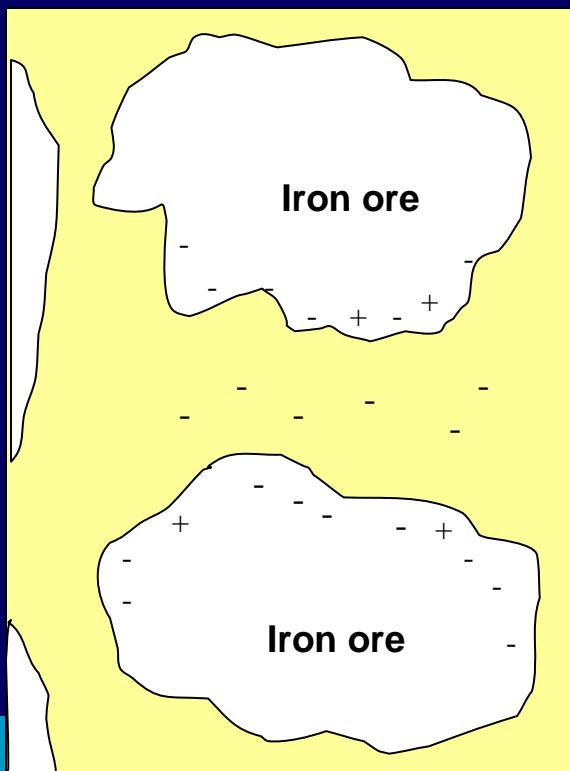
# Feed preparation

- Proper size range!  $65\% < 80 \mu\text{m}$
- Blaine  $1100 - 2500 \text{ cm}^2/\text{g}$
- Optimum moisture  $8.5\%$  for iron ore
  - Higher for a finer smaller feed
- Bentonite as binder and flux additives are common

# Balling principles

- Forces that bind green balls:
  - capillary forces in the liquid film
  - adhesion and cohesion forces
  - attraction between solid particles by van der Waal and electrostatic forces
  - mechanical interlocking of the granular particles
- Binders:
  - soluble salts,
  - bentonite,
  - inorganic chemicals,
  - organic materials.

# Principle of balling

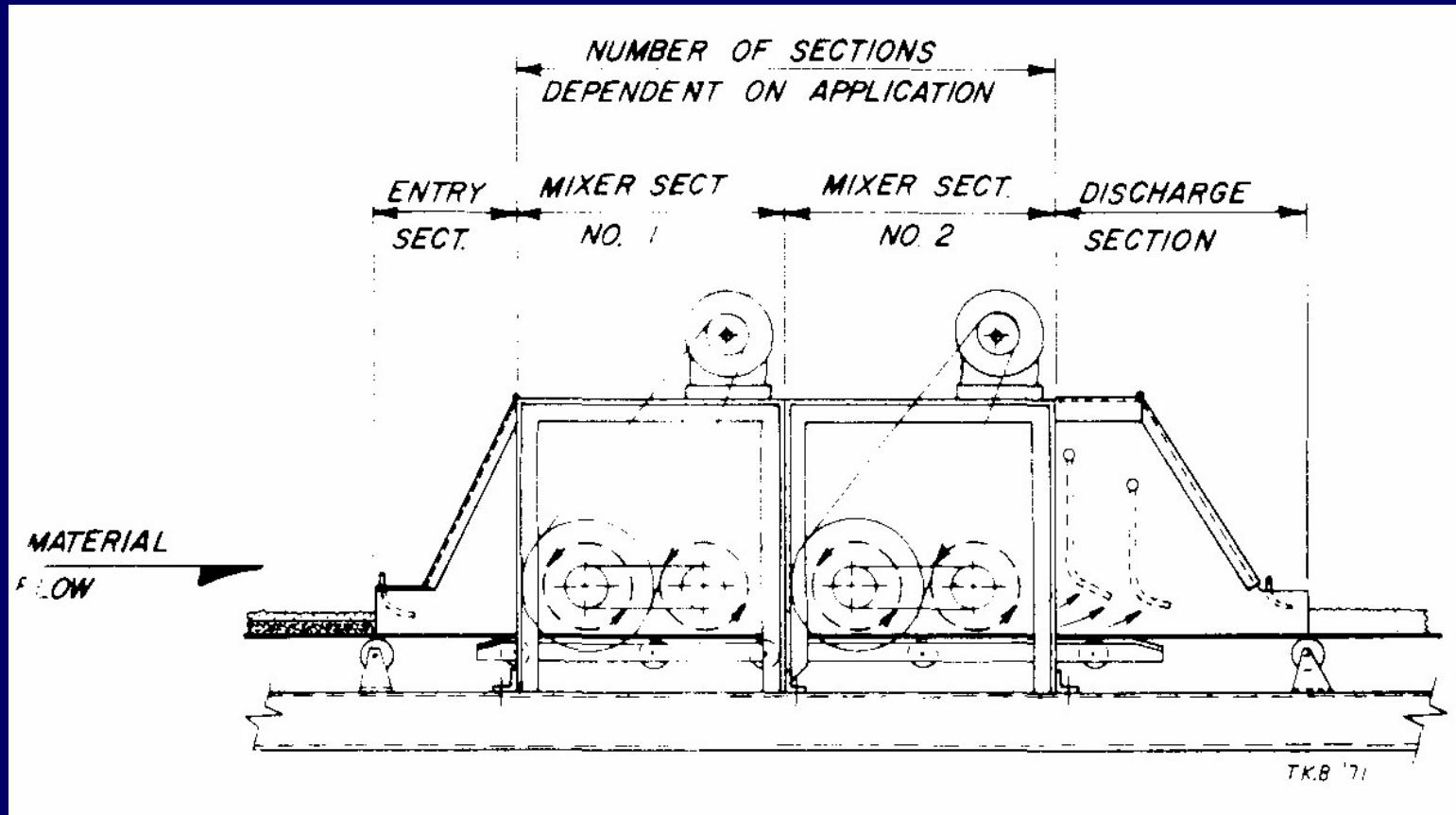


# Important

- uniform size distribution of feed,
- uniform balling feed mixture,
- uniform addition of additives,
- good mixing of additives,
- maintaining clean screening surfaces

# Feed mixing

## Belt mixer



# Balling disc



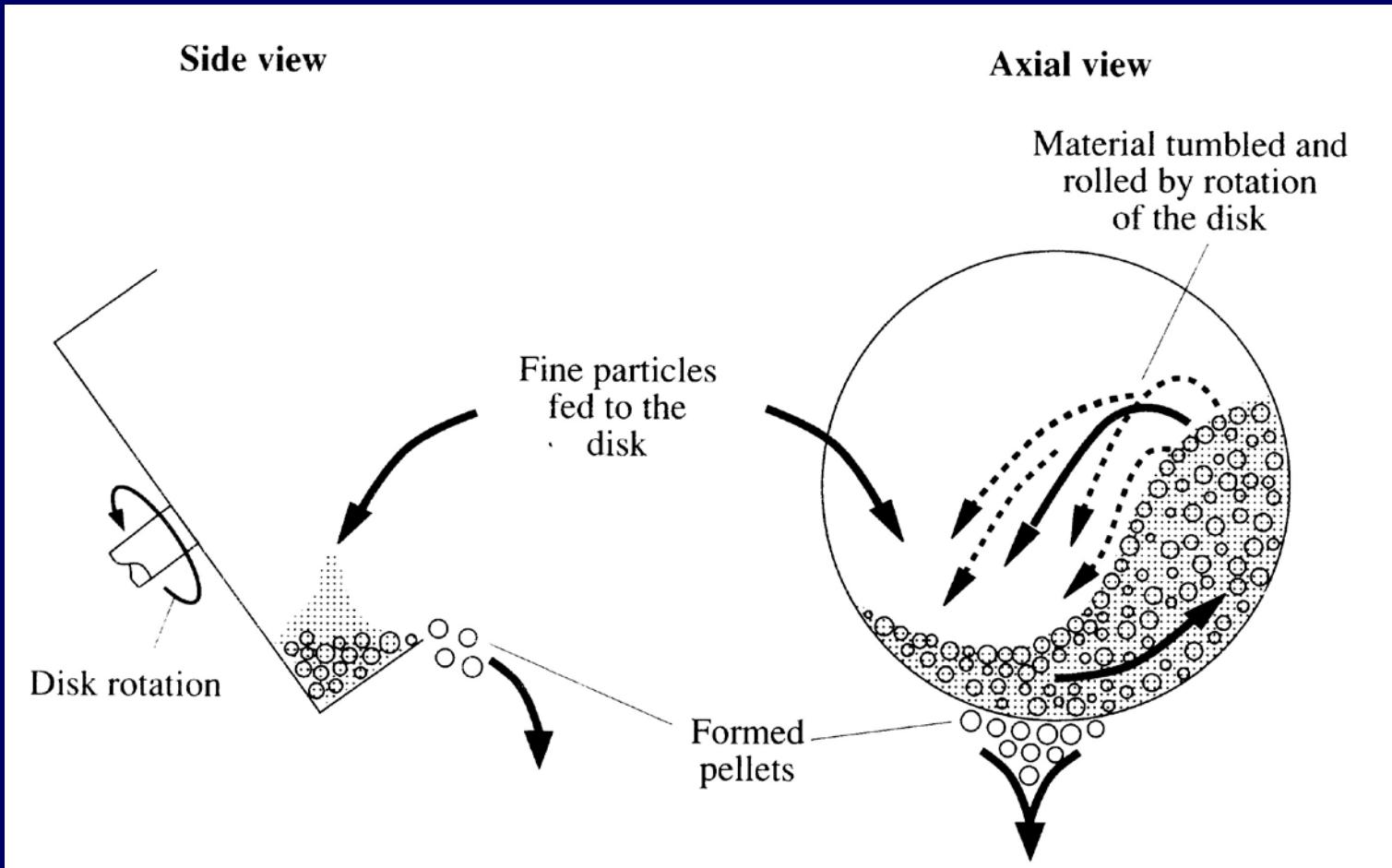
- Natural size classification



# Balling disc with roller screen



# Balling pan principle

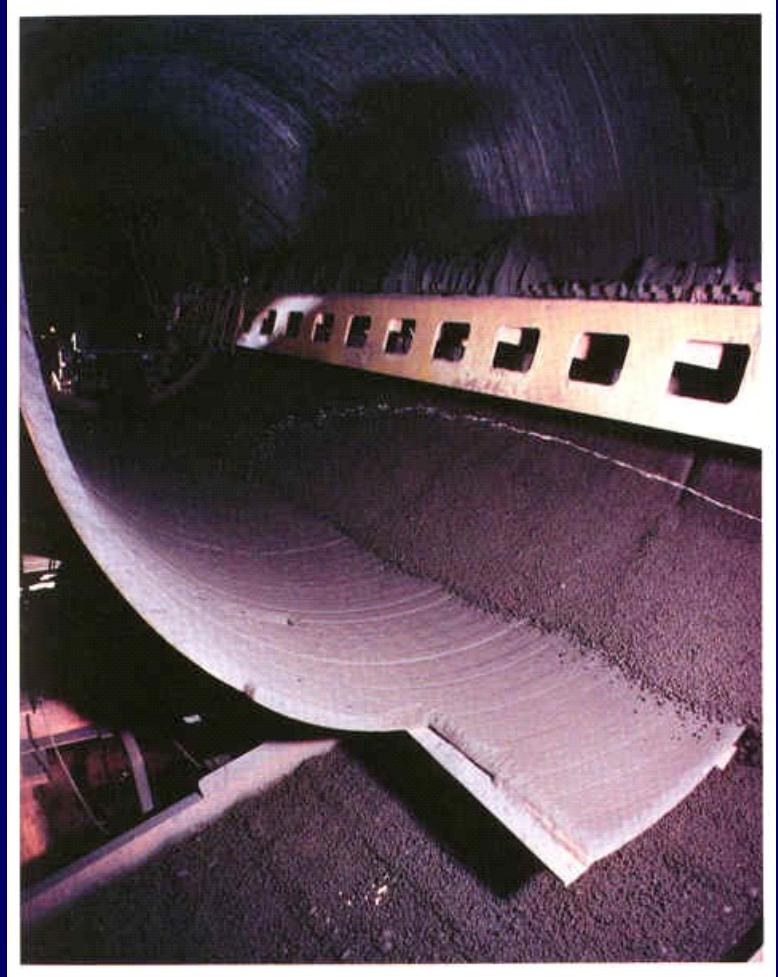


# Balling pan data

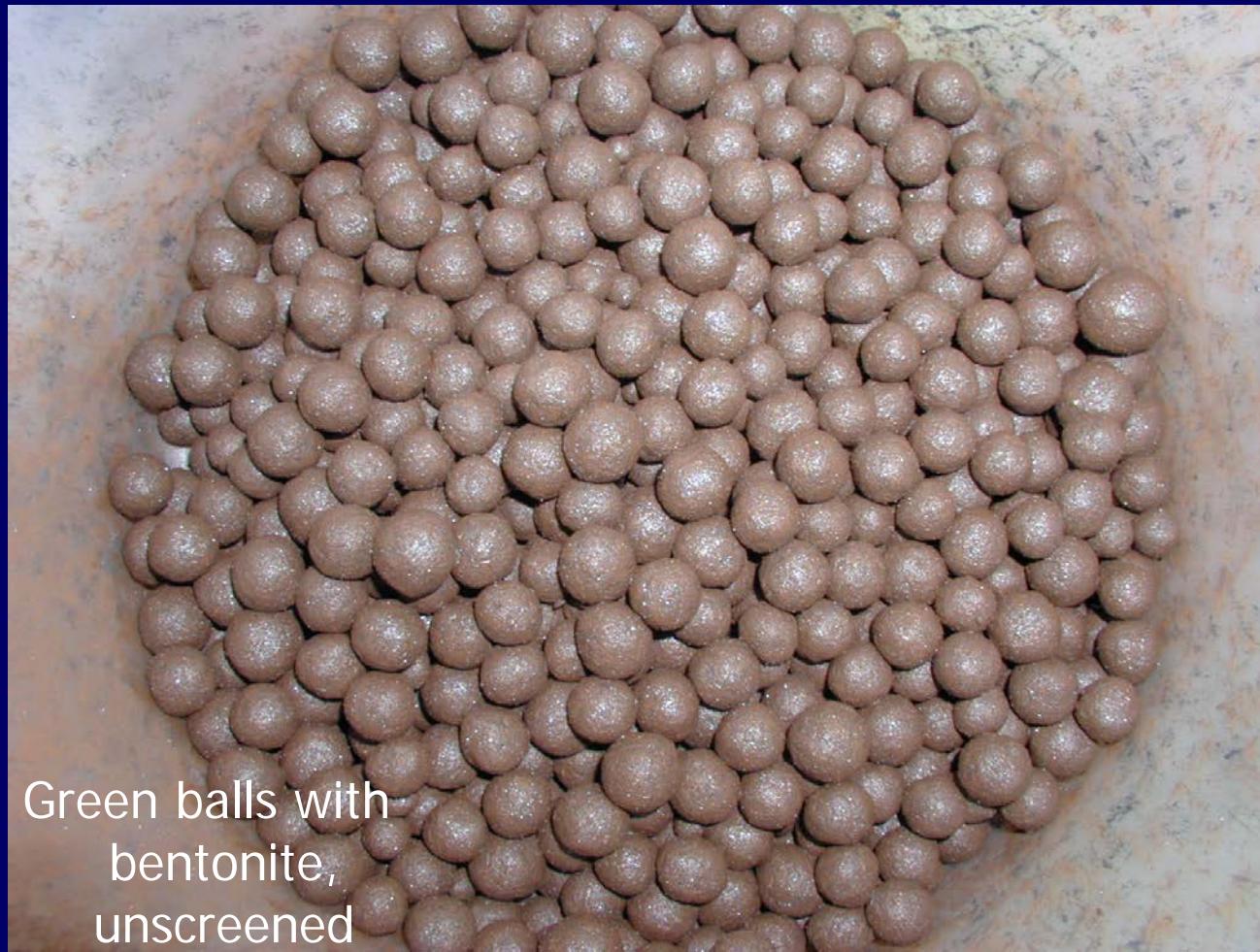
<i>Size: inner diam. (m)</i>	<i>Rotation speed (rpm)</i>	<i>Output (t/h magnetite)</i>
4.5	9.0	60
6.3	7.5	80
7.59	6.2	120

# Balling drum

- Operated in closed circuit
- Easier to control



# Green balls

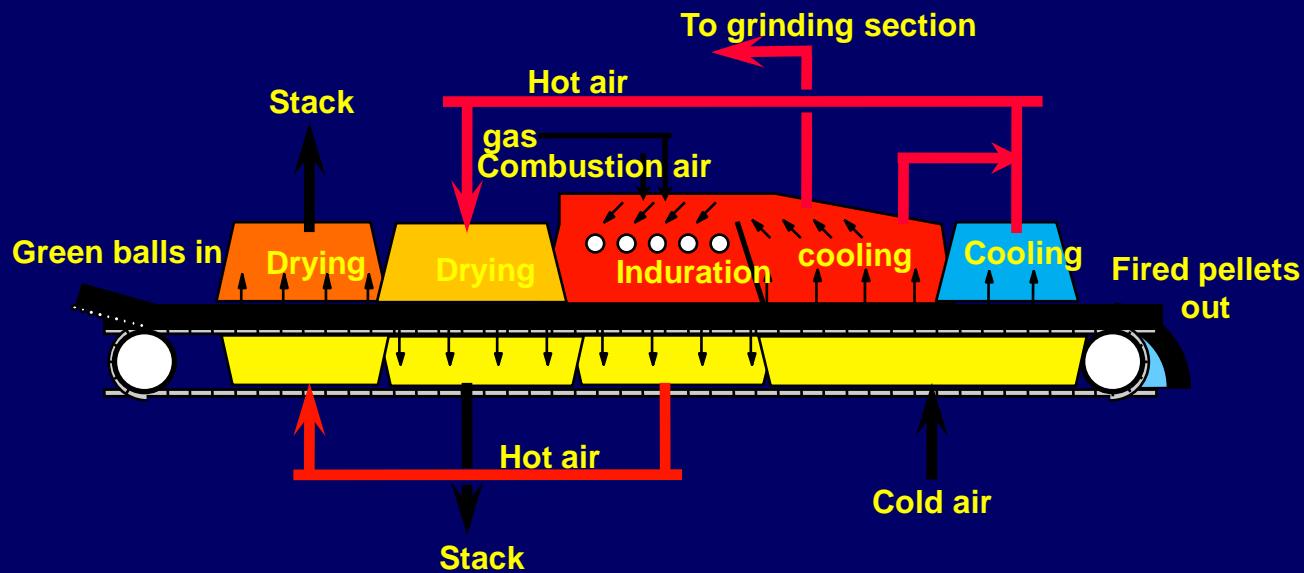


# Balling drum data

<i>Size: diam. x length (m)</i>	<i>Rotation speed (rpm)</i>	<i>Output (t/h magnetite)</i>
2.7 x 9.3	12.0	60
3.0 x 9.6	11.2	80
3.6 x 9.9	9.3	120

# Straight grate induration machine: principle

$430 \text{ m}^2 = 30 \text{ t/m}^2 24 \text{ hr}$



# Grate kiln



December 2012

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# Induration Process

## Bed permeability

The permeability or void fraction of a packed bed of pellets is a critical parameter for the productivity, energy efficiency and stable operation of:

- Induration furnaces
- Blast furnaces
- DR shafts

# Induration Process

## Bed permeability

Pressure drop across a packed bed of spheres

Ergun equation:

$$\Delta P = \left[ \frac{150(1-\varepsilon)^2 \mu_g}{\Phi^2 d^2 \varepsilon^3 e_g} G + \frac{1.75(1-\varepsilon)}{\Phi d \varepsilon^3 e_g} G^2 \right] \Delta Z$$

# Induration Process

## Bed permeability

Pressure drop across a packed bed of spheres

Ergun equation:

Everything else being constant, approximately:

$$\Delta P \propto \frac{1}{\varepsilon^3}$$

# Induration Process

## Bed permeability

$$\Delta P \propto \frac{1}{\varepsilon^3}$$

$\varepsilon$  = Void fraction = 0.37 to 0.43

If  $\Delta\varepsilon = 0.02$

$\Delta P \approx 15\%$

$\Delta G \approx 8\%$  (productivity)

# Induration Process

## Bed permeability

$$\Delta P \propto \frac{1}{\varepsilon^3}$$

$$\varepsilon \propto \text{Green ball plasticity} \propto \begin{array}{l} \text{H}_2\text{O} \\ \text{Binder} \\ \text{Ore particle size} \end{array}$$
$$\varepsilon \propto \text{Bed Packing} \propto \begin{array}{l} \text{Ball size dist.} \\ \text{Sphericity} \\ \text{Feeding device} \end{array}$$