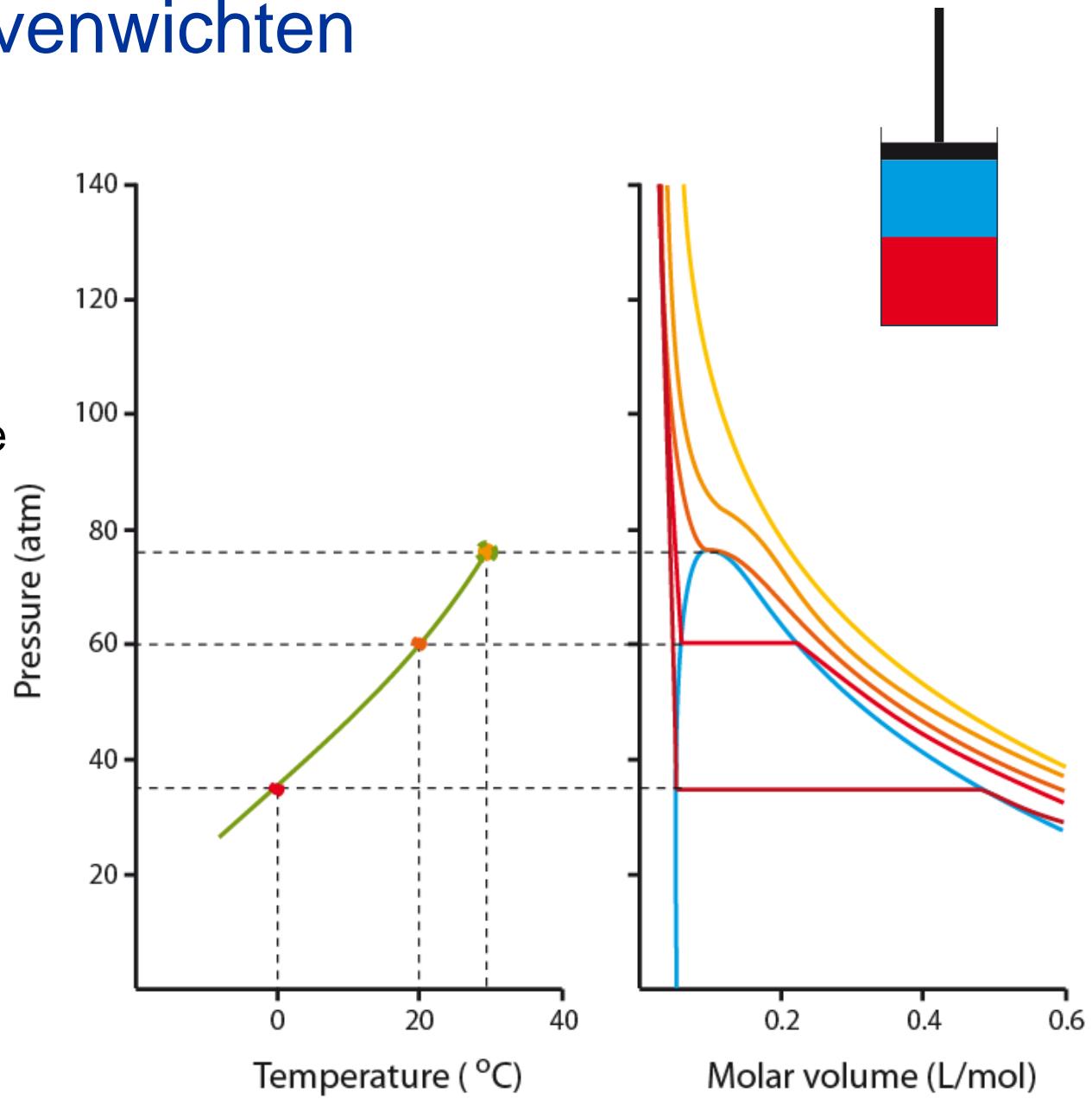


Fasenevenwichten van mengsels

Vloeistof-dampevenwichten

Zuivere stoffen

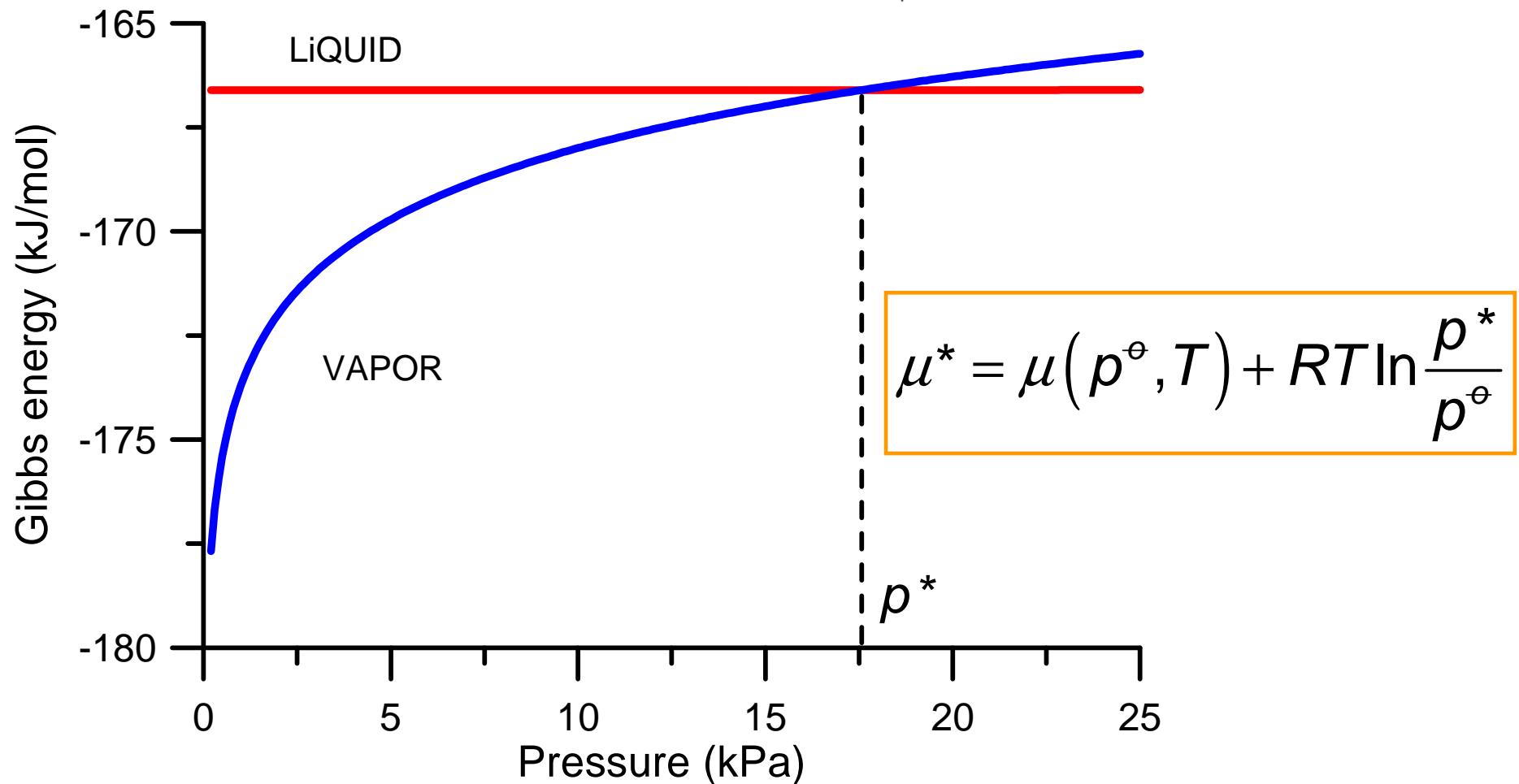
- dampspanning
- extensieve variabele
 - 2-fasengebied
- “hefboom”-regel



Vloeistof-dampevenwichten

Dampspanning (voorbeeld methanol)

Form	$\Delta_f G^\ominus$ (kJ/mol)	S^\ominus (J/(K mol))	V_m (cm ³ /mol)
liquid	-166.6	126.8	40.5
vapor	-162.3	239.9	—



Vloeistof-dampevenwichten



John Dalton (1766 – 1844)

Wet van Dalton

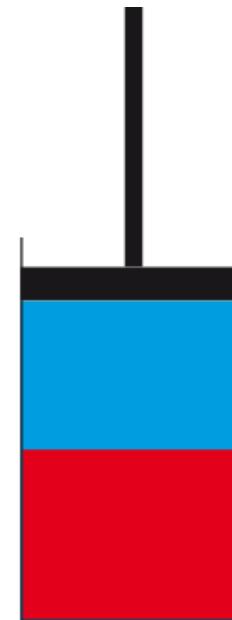
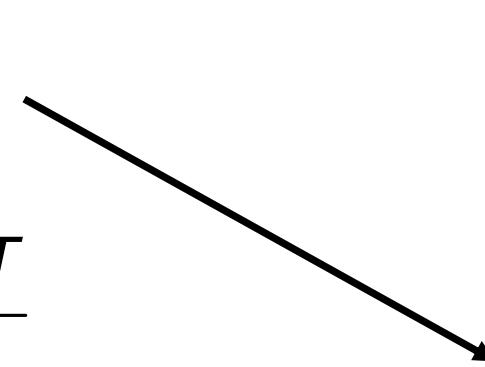
$$p_j = y_j p$$

Molfractie

$$y_j = \frac{n_j}{n}$$

Partiële druk

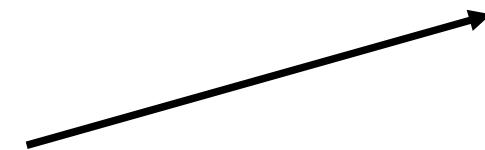
$$p_j = \frac{n_j R T}{V}$$



Vloeistofmengsels

Molfractie

$$x_j = \frac{n_j}{n}$$



Vloeistof-dampevenwichten

Kooklijn: wet van Raoult

$$p_j = x_j p_j^*$$



François Raoult (1830 – 1901)

Chemische potentiaal is hetzelfde $\mu_{j,v} = \mu_{j,l}$

Voor de vloeistof:

$$\mu_{j,l} = \mu^\theta_{j,l} + RT \ln x_j$$

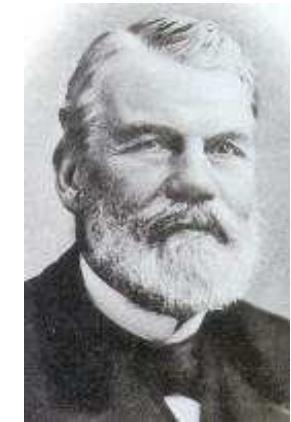
Voor de damp:

$$\mu_{j,v} = \mu^\theta_{j,v} + RT \ln \frac{p_j}{p^\theta}$$

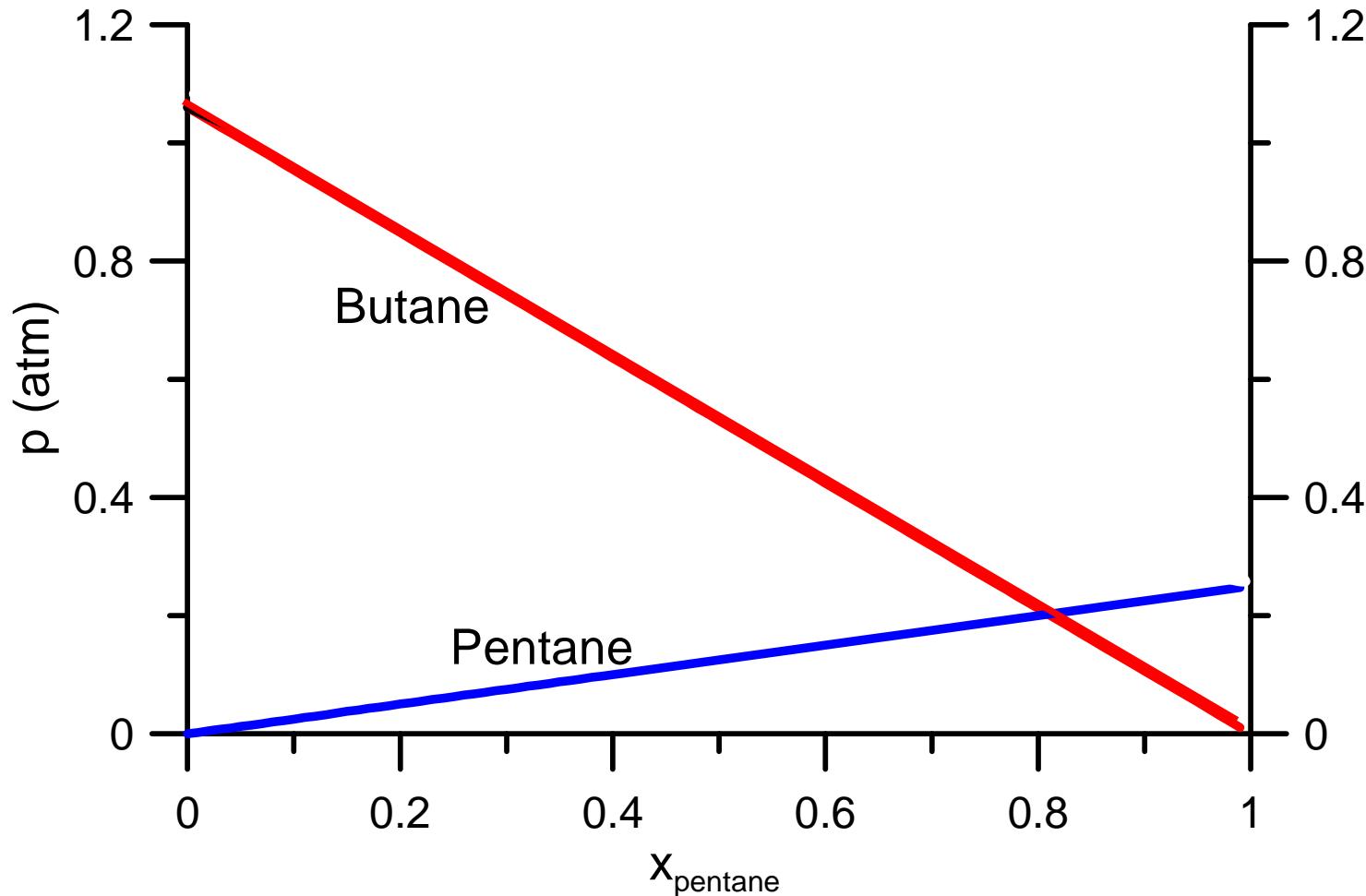
$$\mu^\theta_{j,l} + RT \ln x_j = \mu^\theta_{j,v} + RT \ln \frac{p_j}{p^\theta}$$

Vloeistof-dampevenwichten

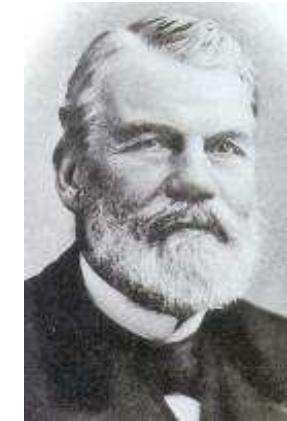
Kooklijn: wet van Raoult $p_j = x_j p_j^*$



François Raoult (1830 – 1901)

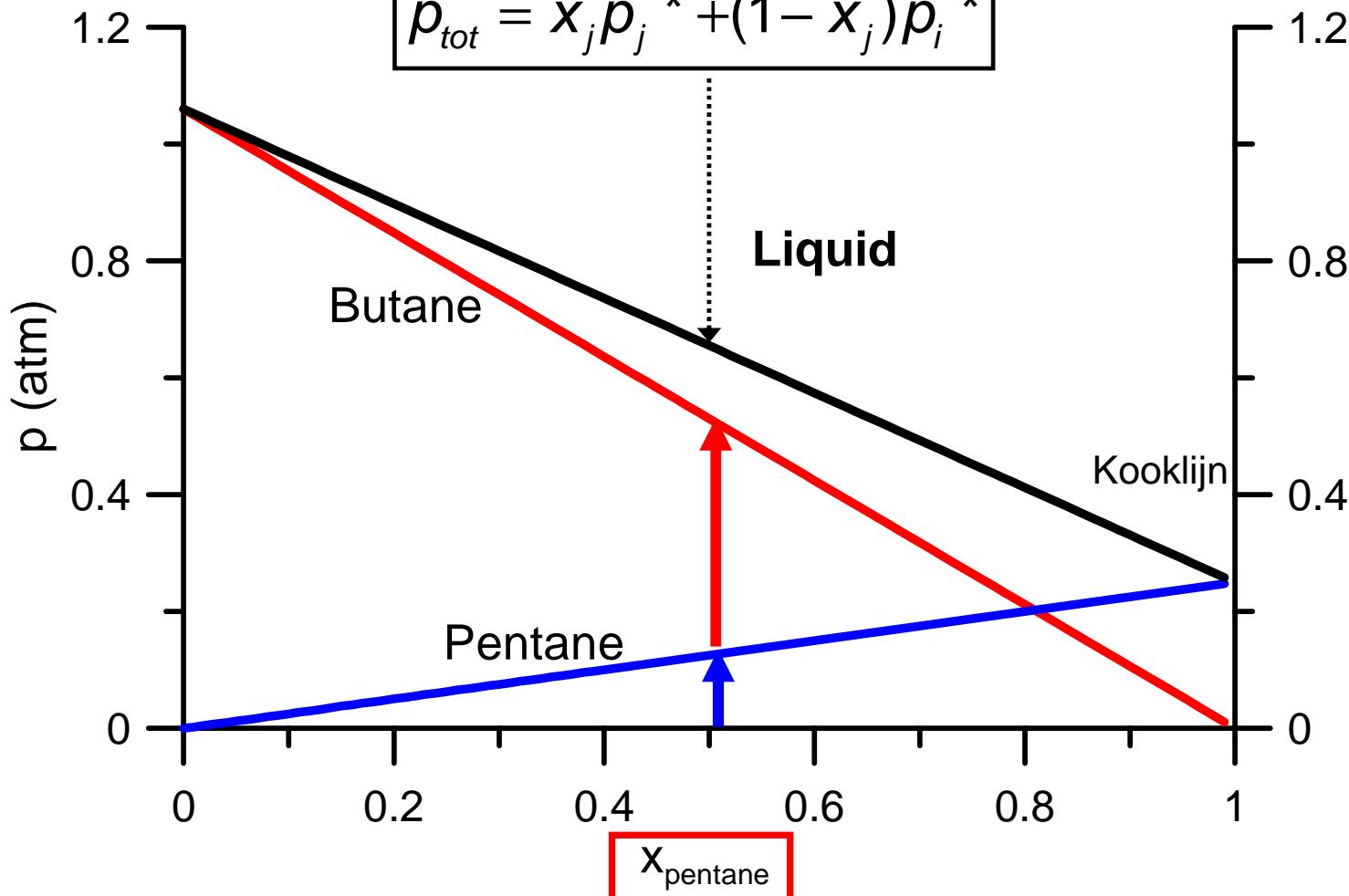


Vloeistof-dampevenwichten



Kooklijn: wet van Raoult $p_j = x_j p_j^*$

$$p_{tot} = x_j p_j^* + (1 - x_j) p_i^*$$



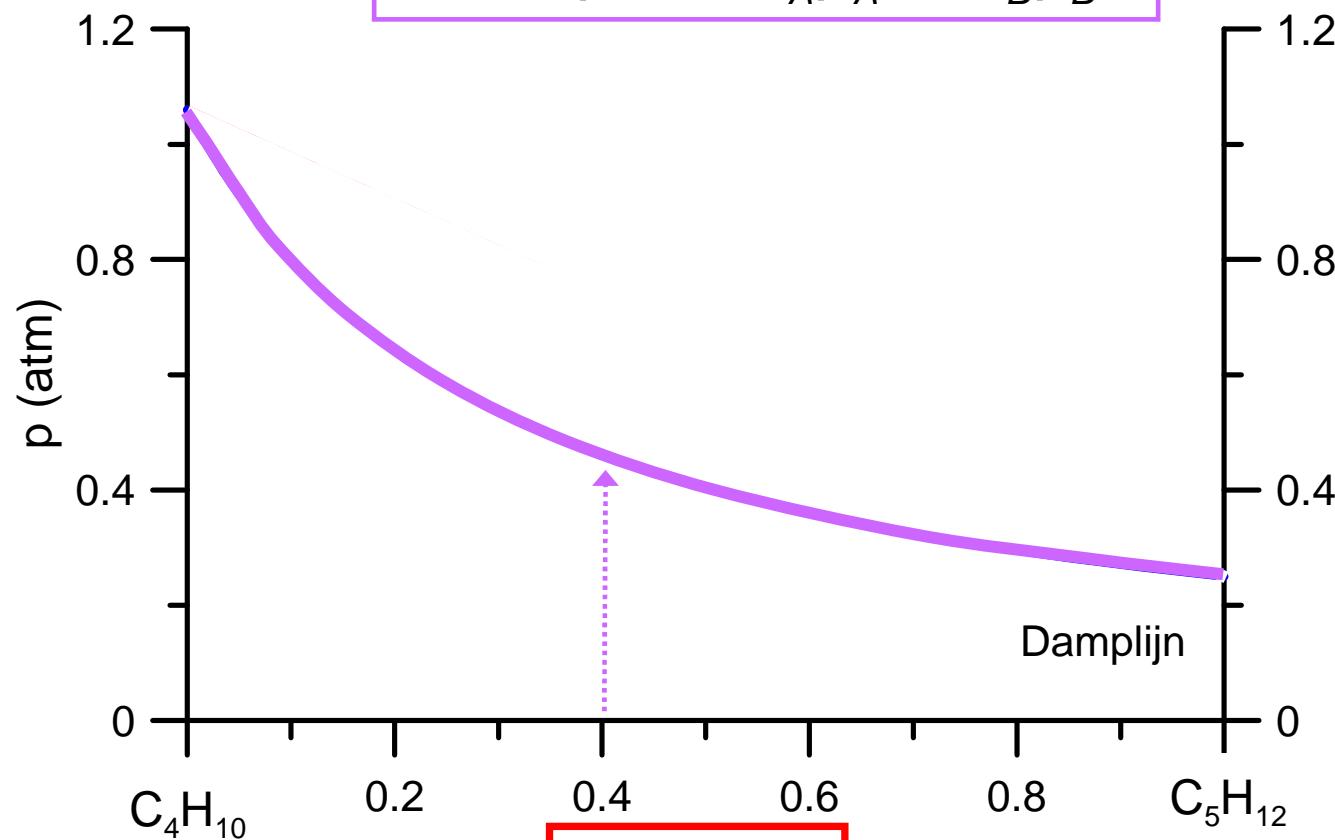
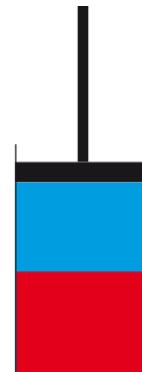
Vloeistof-dampevenwichten

$$p_j = x_j p_j^*$$

$$p = p_A + p_B = x_A p_A^* + x_B p_B^*$$

Damplijn:

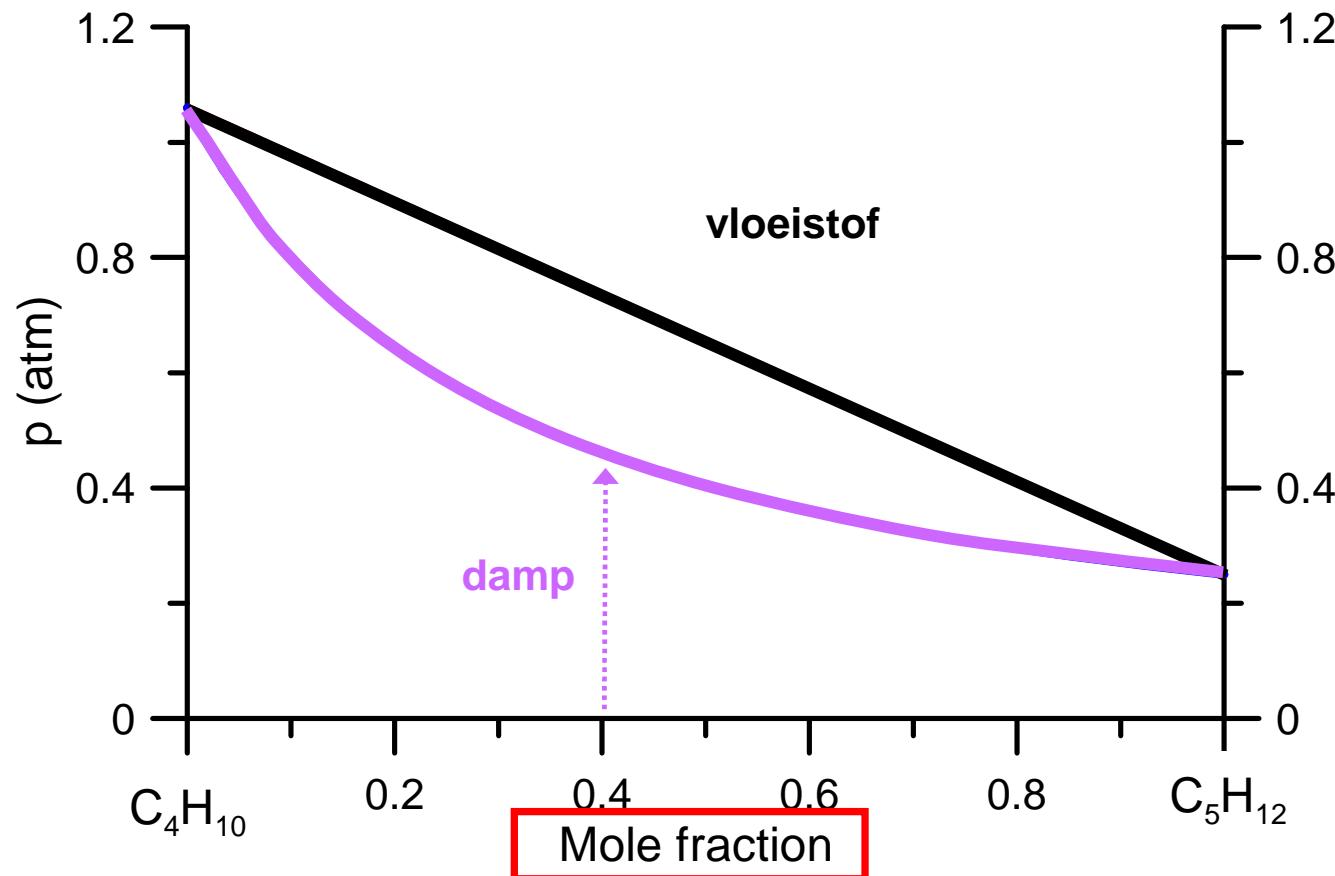
$$y_j = \frac{x_j p_j^*}{p} = \frac{x_j p_j^*}{x_A p_A^* + x_B p_B^*}$$



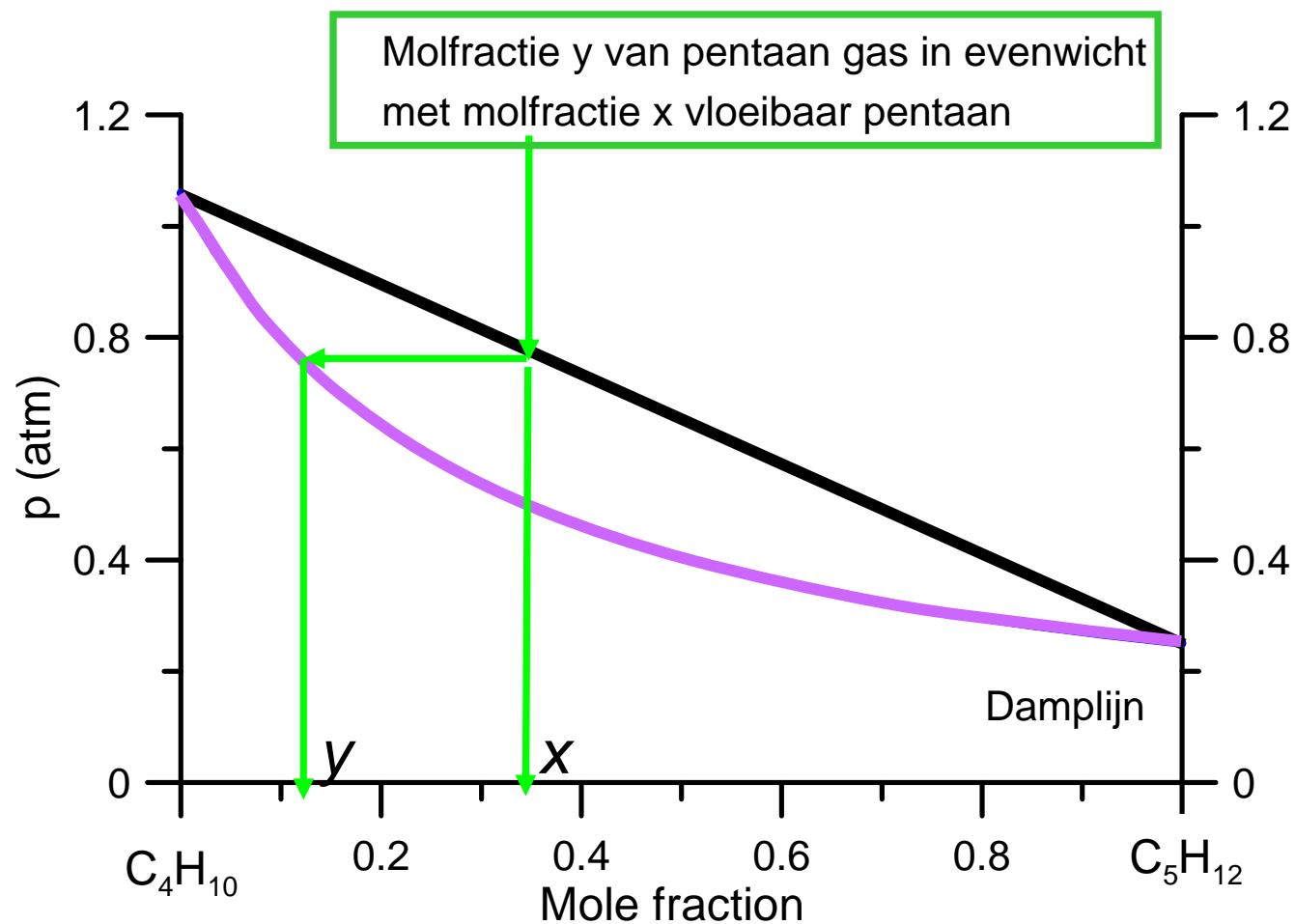
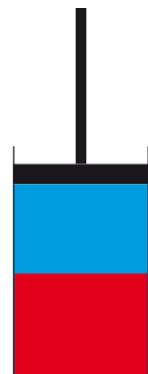
Vloeistof-dampevenwichten

$$p_j = x_j p_j^*$$

$$p = p_A + p_B = x_A p_A^* + x_B p_B^*$$



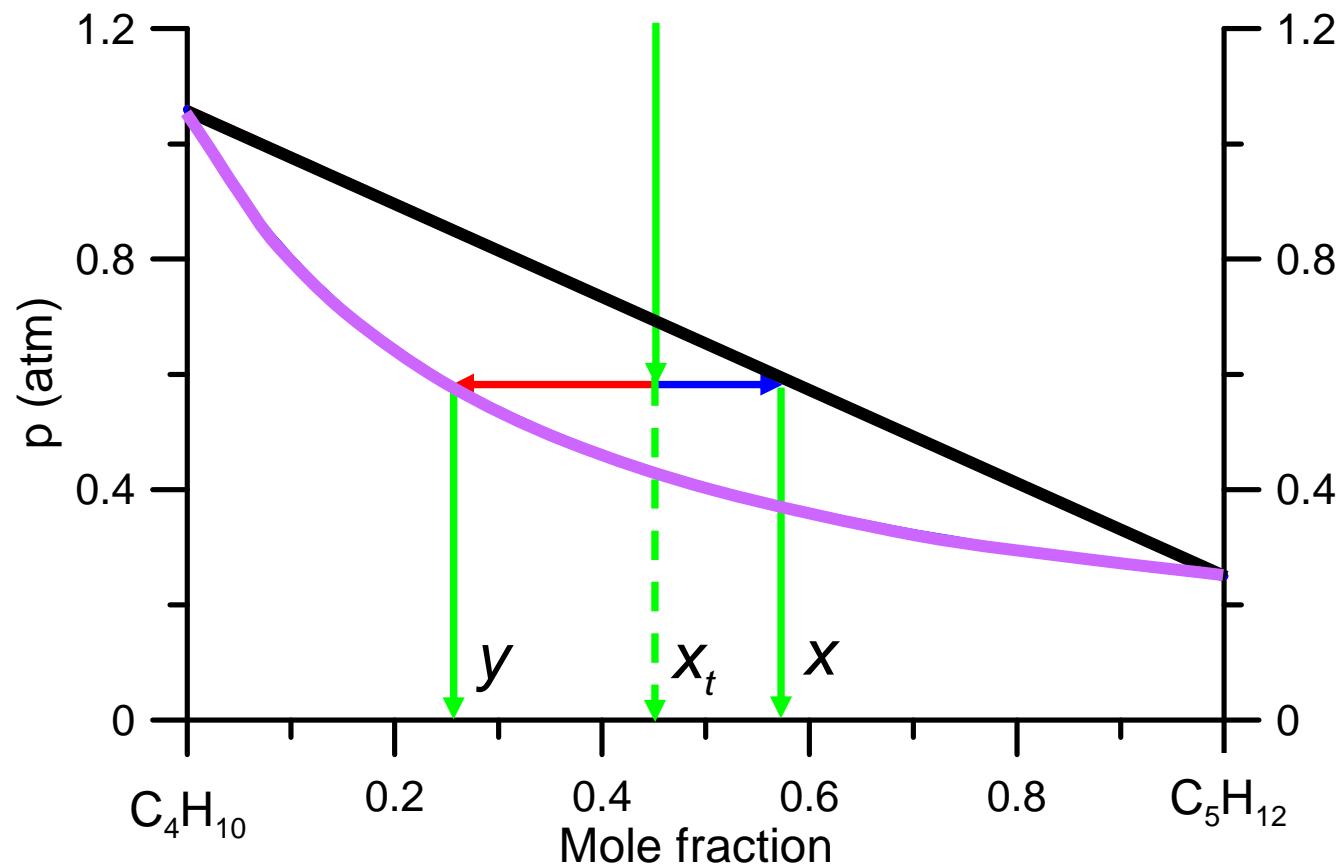
Vloeistof-dampevenwichten



Vloeistof-dampevenwichten

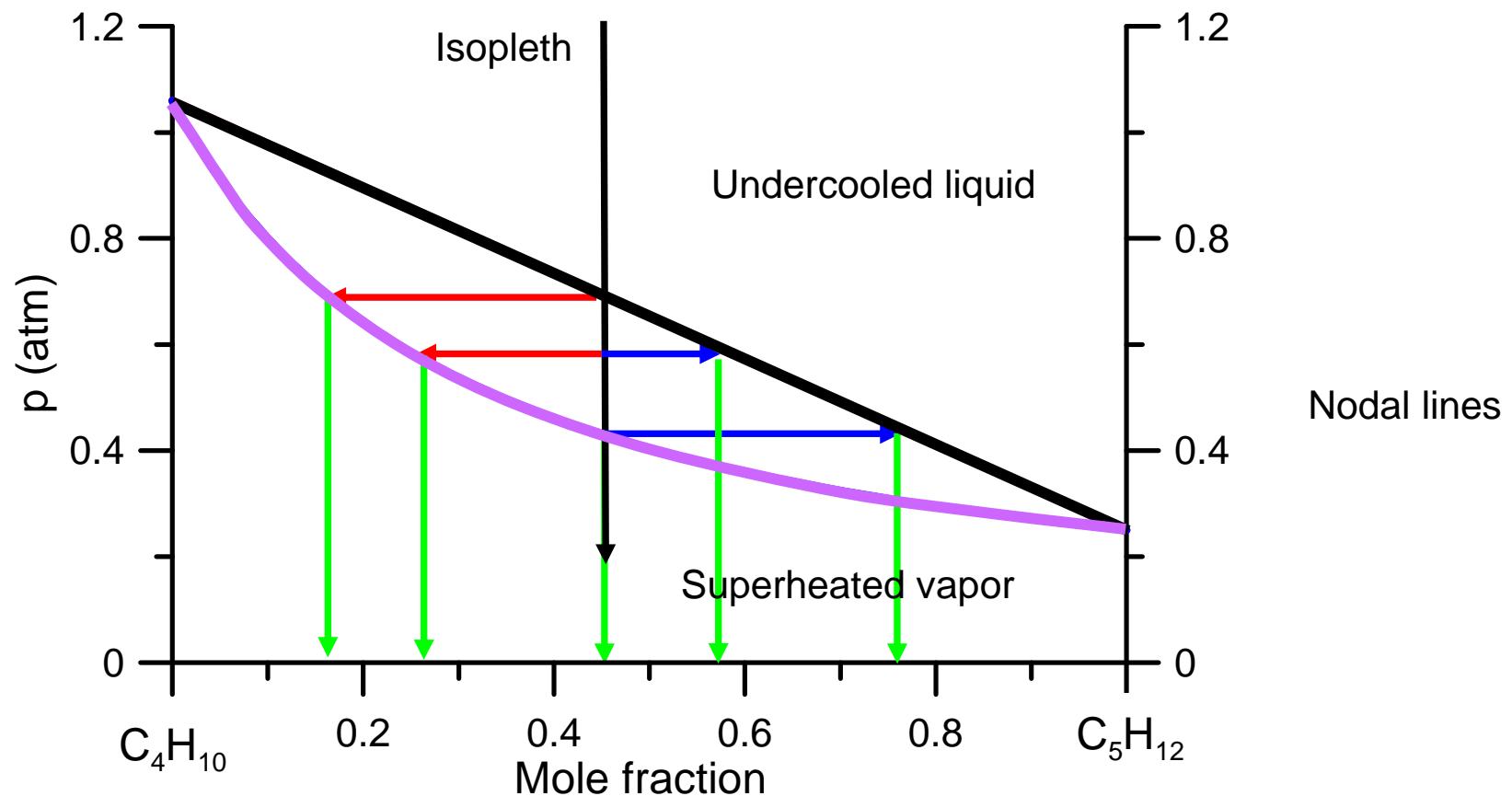
Hefboomregel (lever rule)

$$\frac{n_v}{n_l} = \frac{x_t - x}{y - x_t}$$



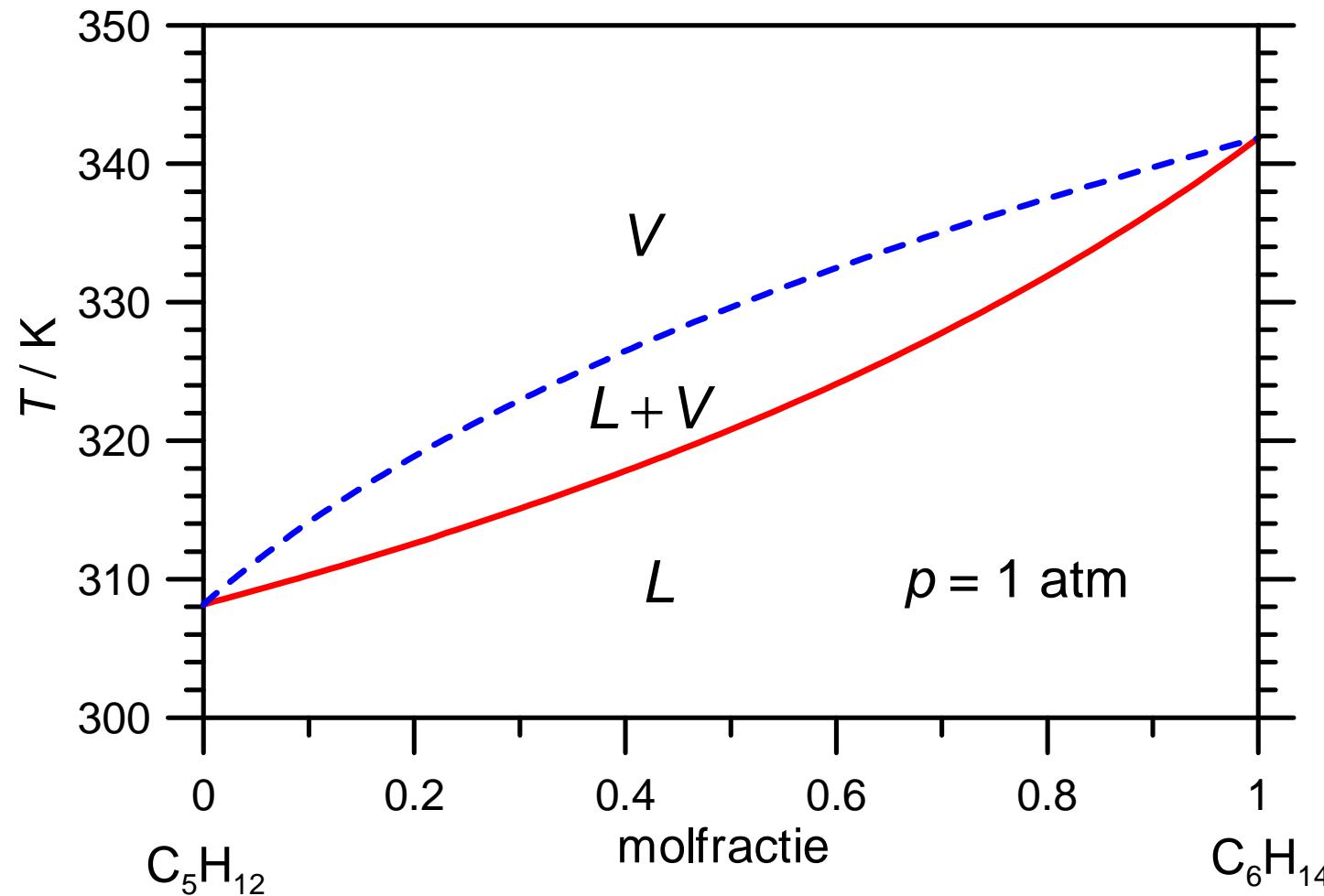
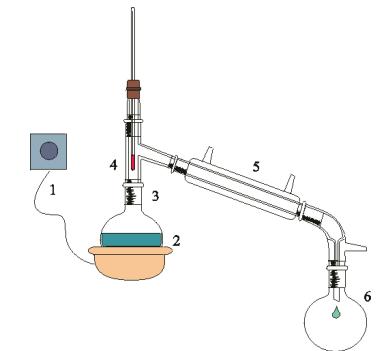
Vloeistof-dampevenwichten

Verdamping door decompressie: interpretatie P-x-diagram



Vloeistof-dampevenwichten

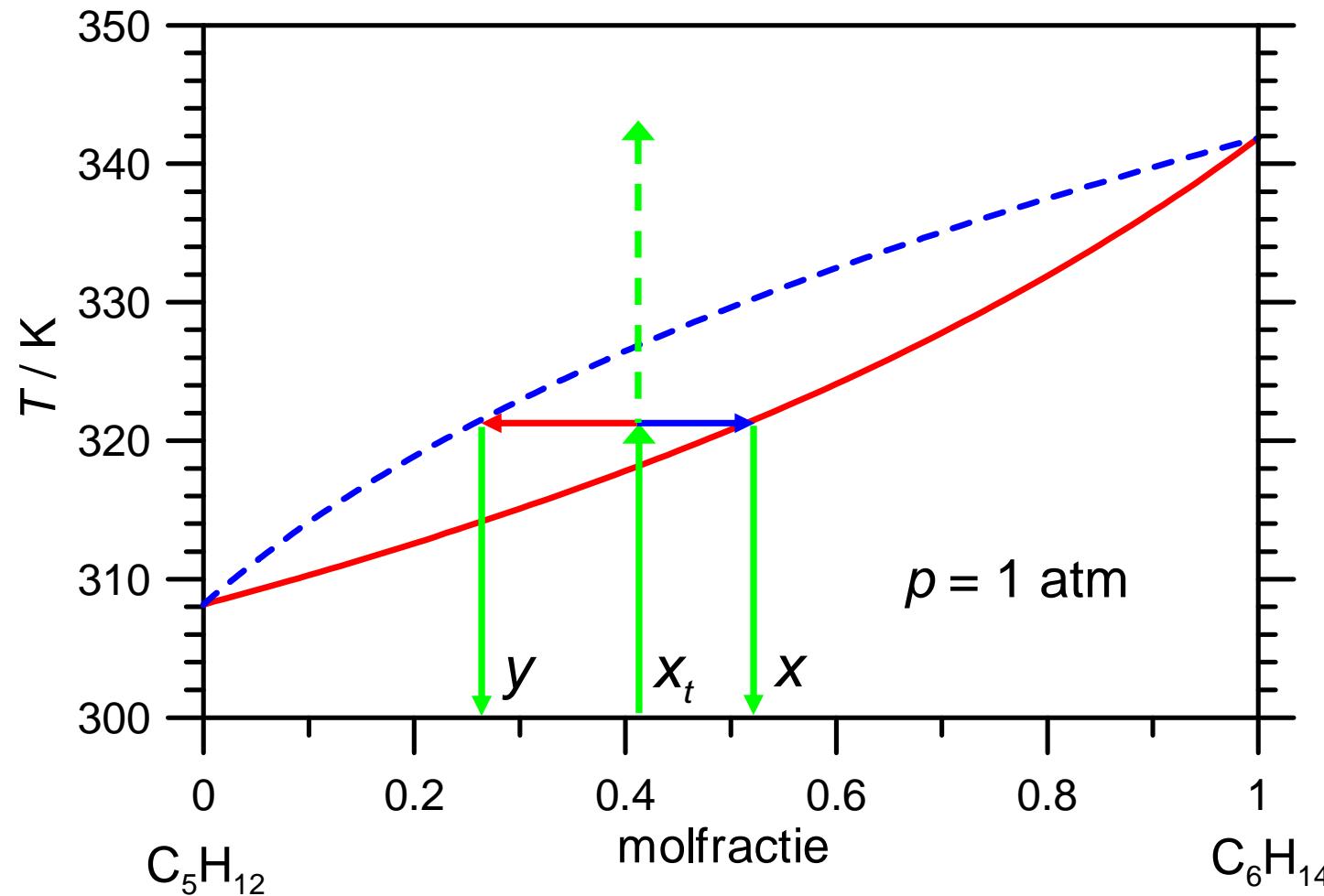
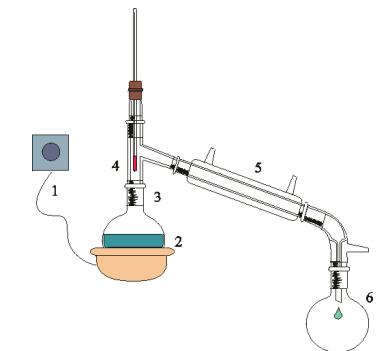
Interpretatie **T-x-diagram**: fasengebieden



Vloeistof-dampevenwichten

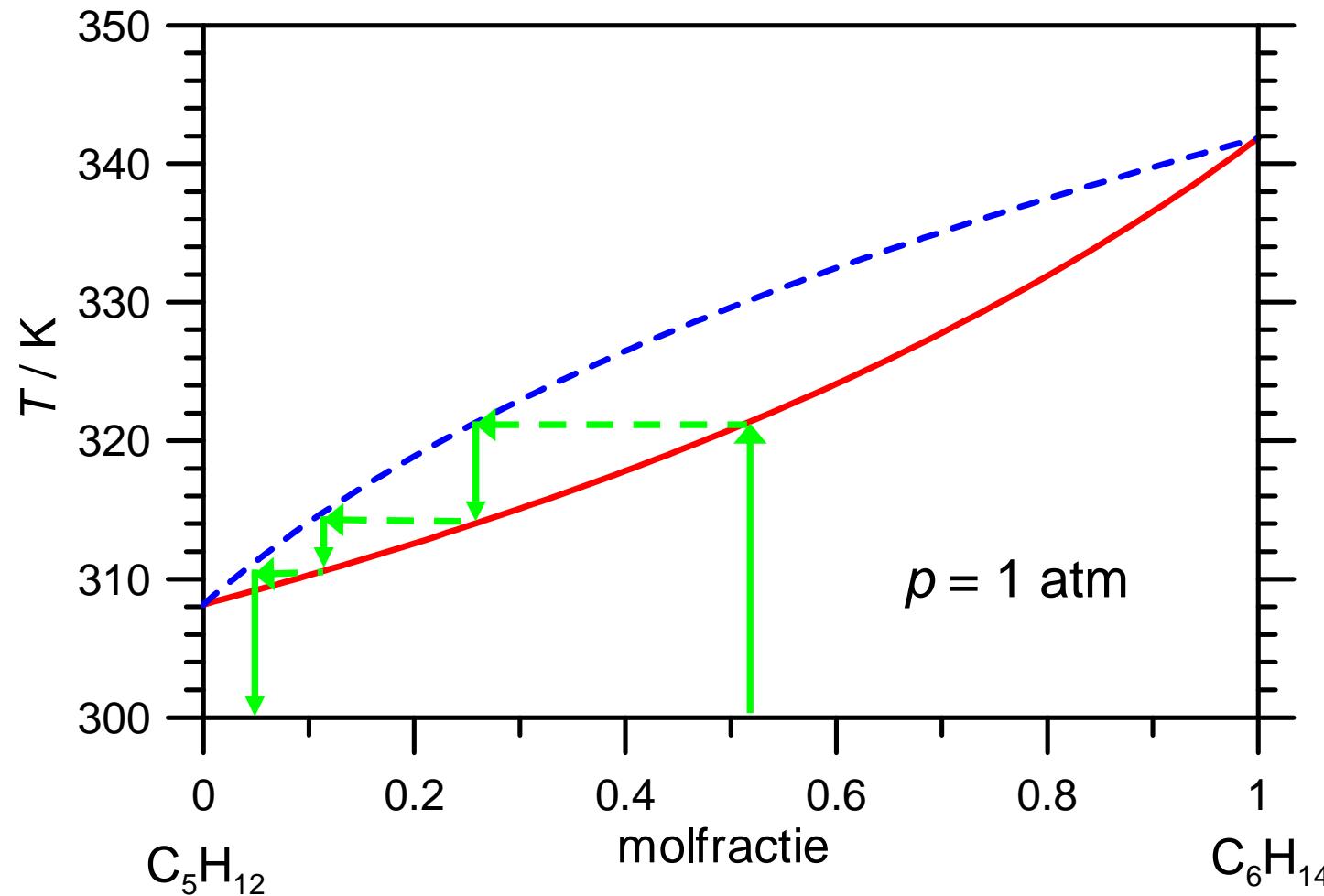
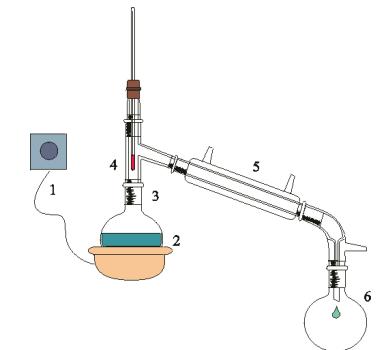
Interpretatie T-x-diagram: hefboomregel

$$\frac{n_v}{n_l} = \frac{x_t - x}{y - x_t}$$



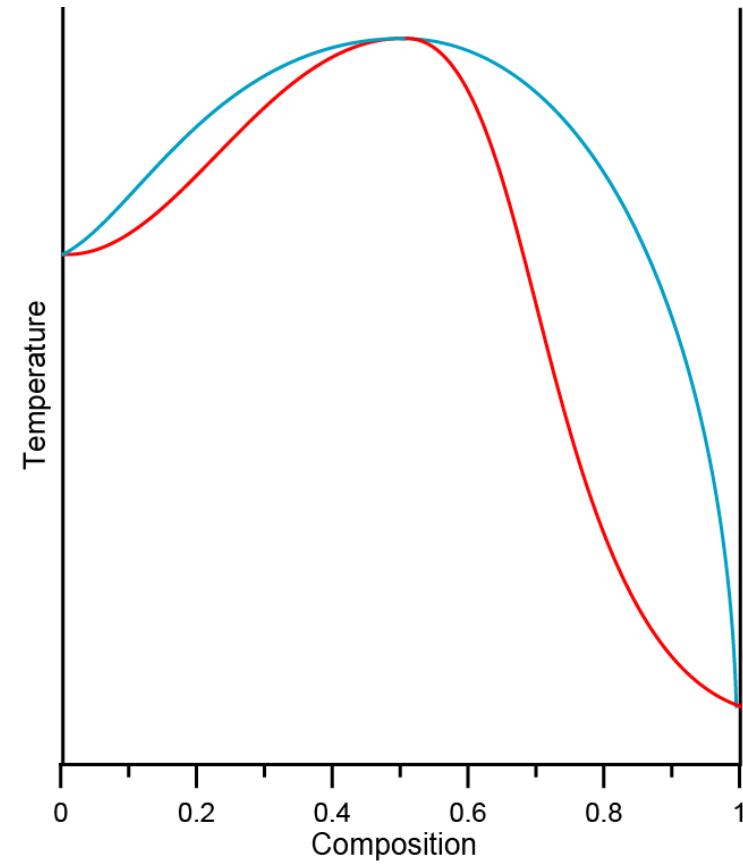
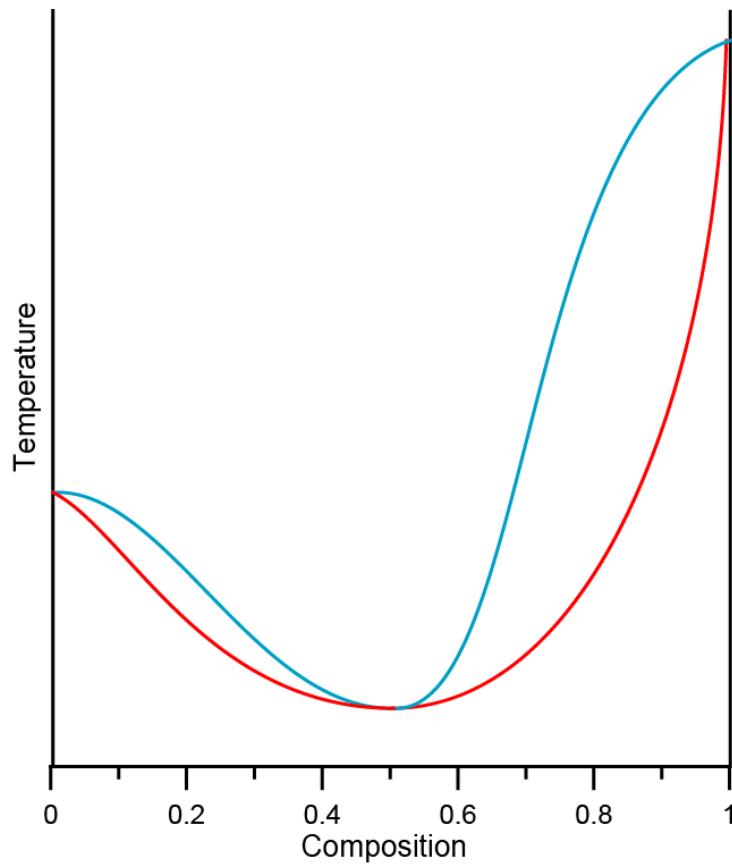
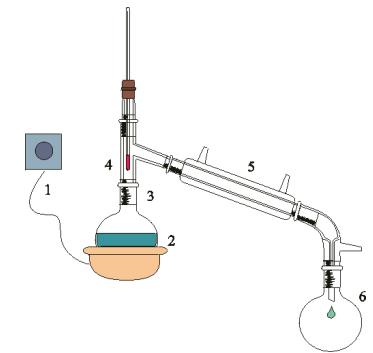
Vloeistof-dampevenwichten

Interpretatie T-x-diagram: destillatie



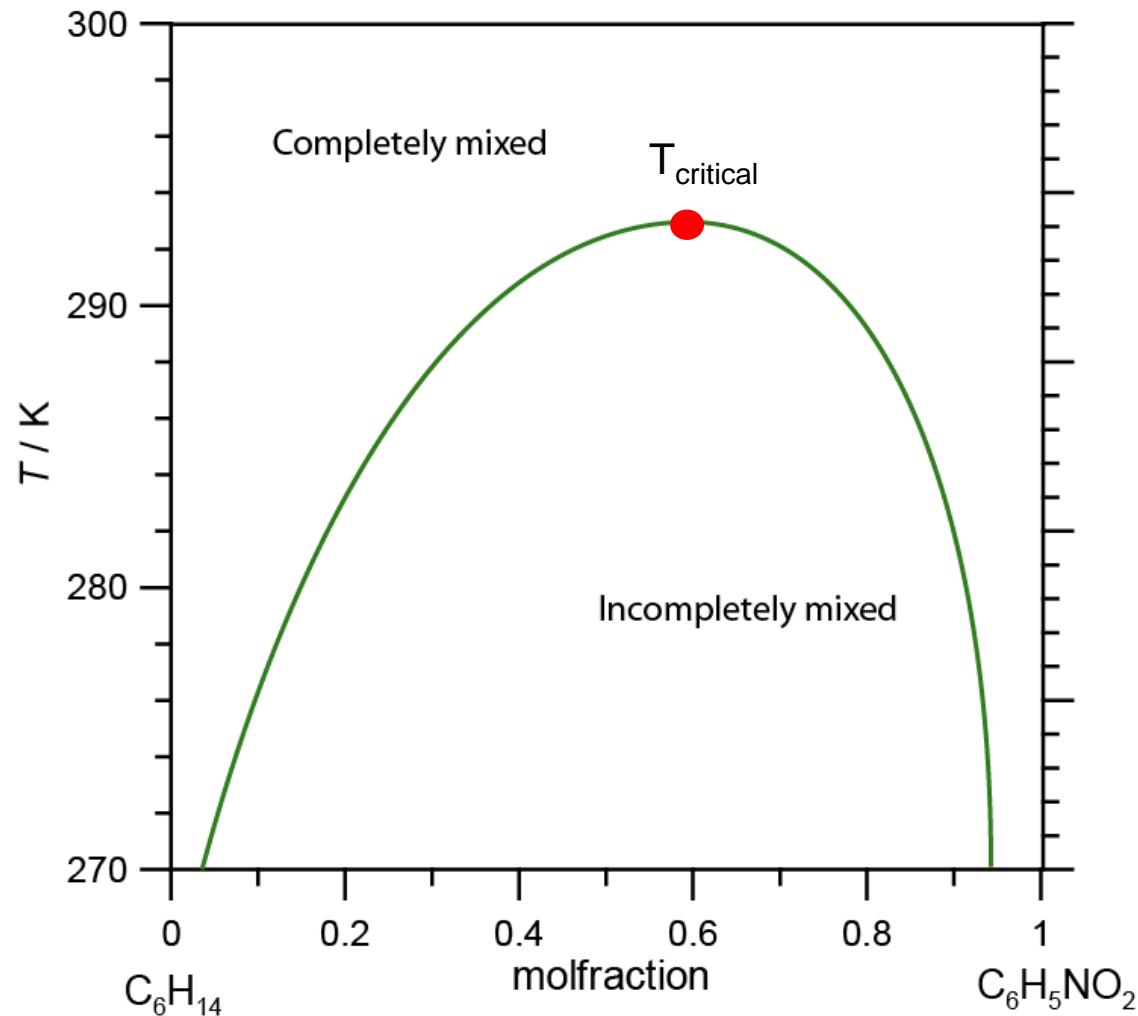
Vloeistof-dampevenwichten

Niet-lineariteiten: azeotropie



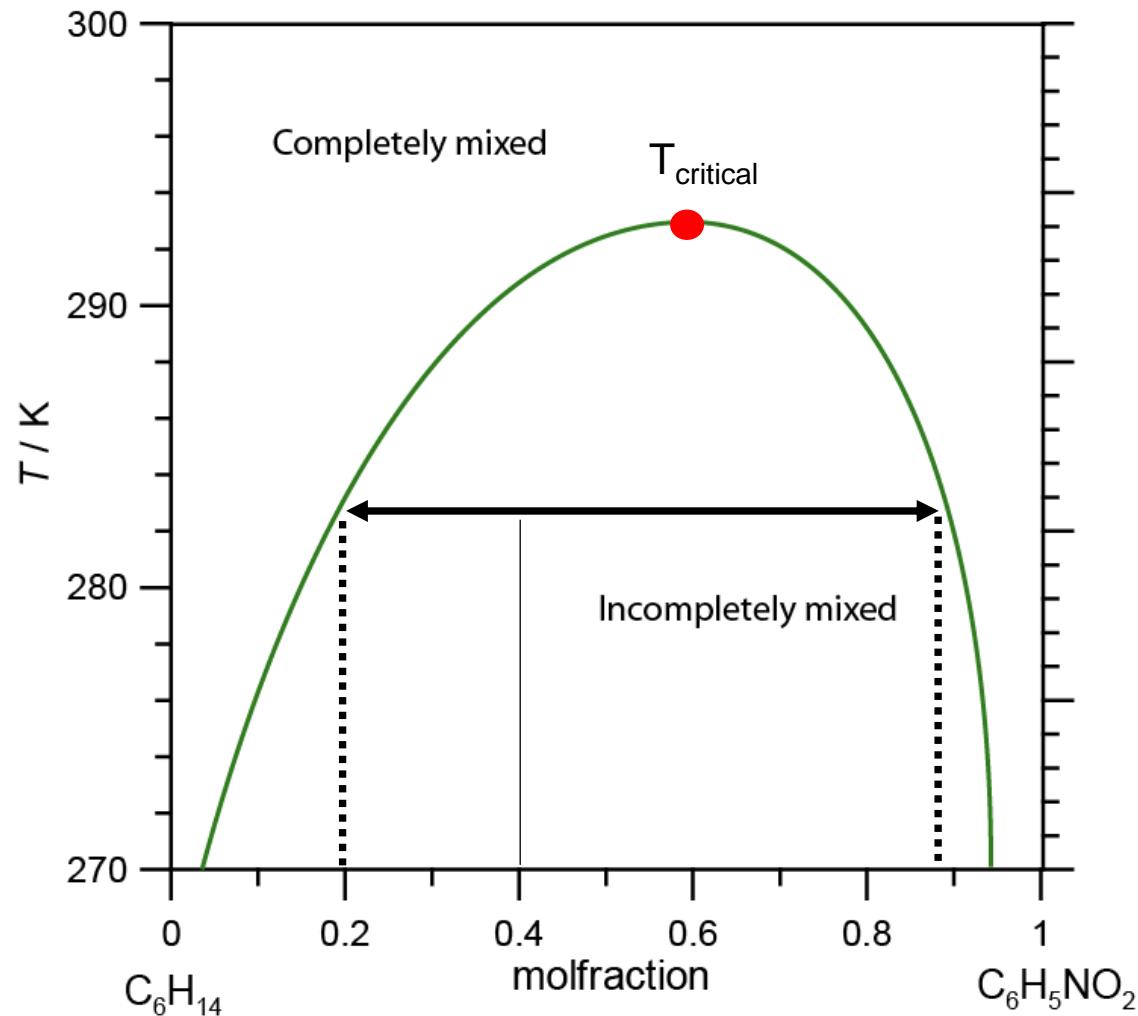
Vloeistof-vloeistof-evenwichten

Gedeeltelijke mengbaarheid (nitrobenzeen in hexaan)



Vloeistof-vloeistof-evenwichten

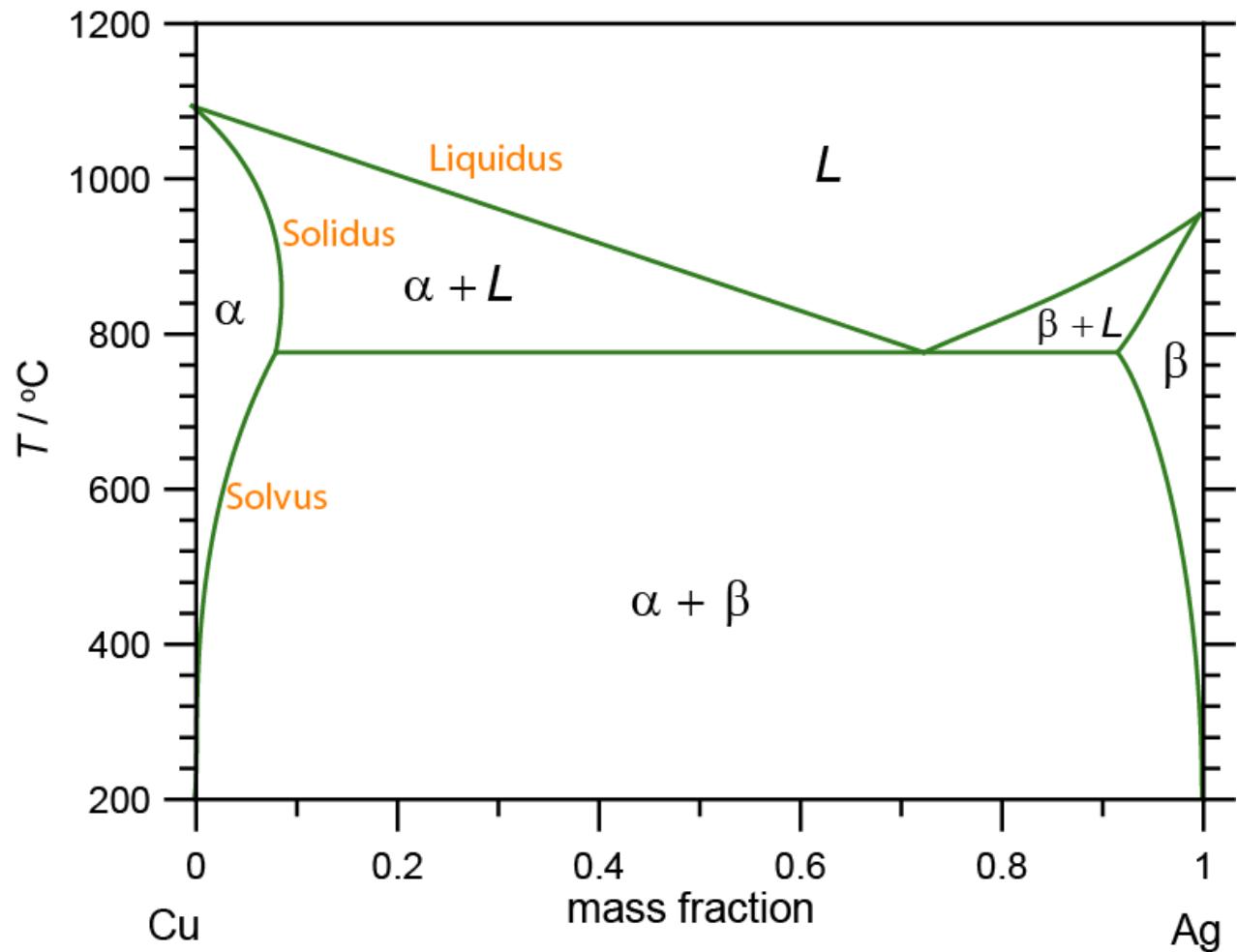
Gedeeltelijke mengbaarheid (nitrobenzeen in hexaan)



Vloeistof-vast-evenwichten

Kenmerken

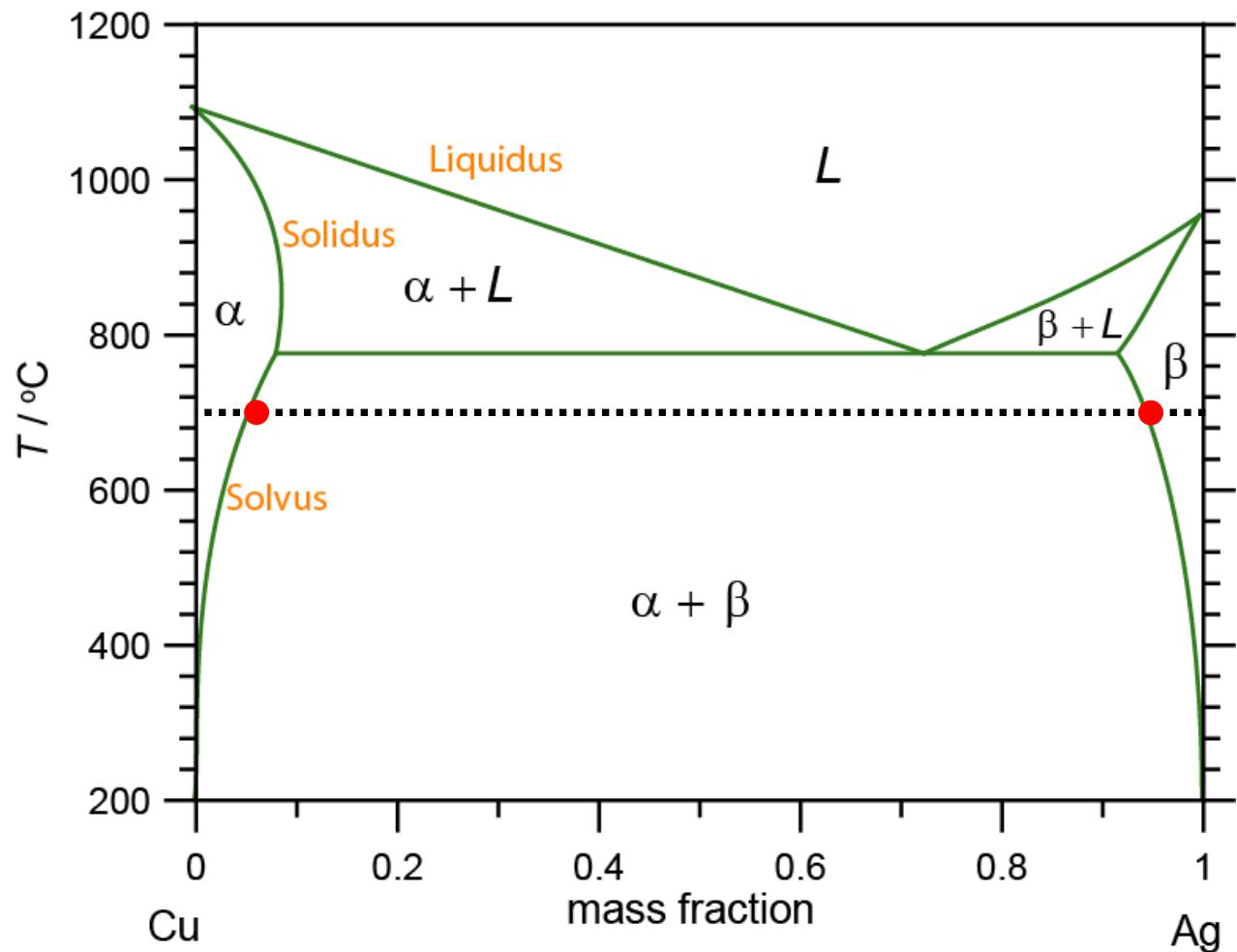
- Eutectisch punt
- oplosbaarheid



Vloeistof-vast-evenwichten

Kenmerken

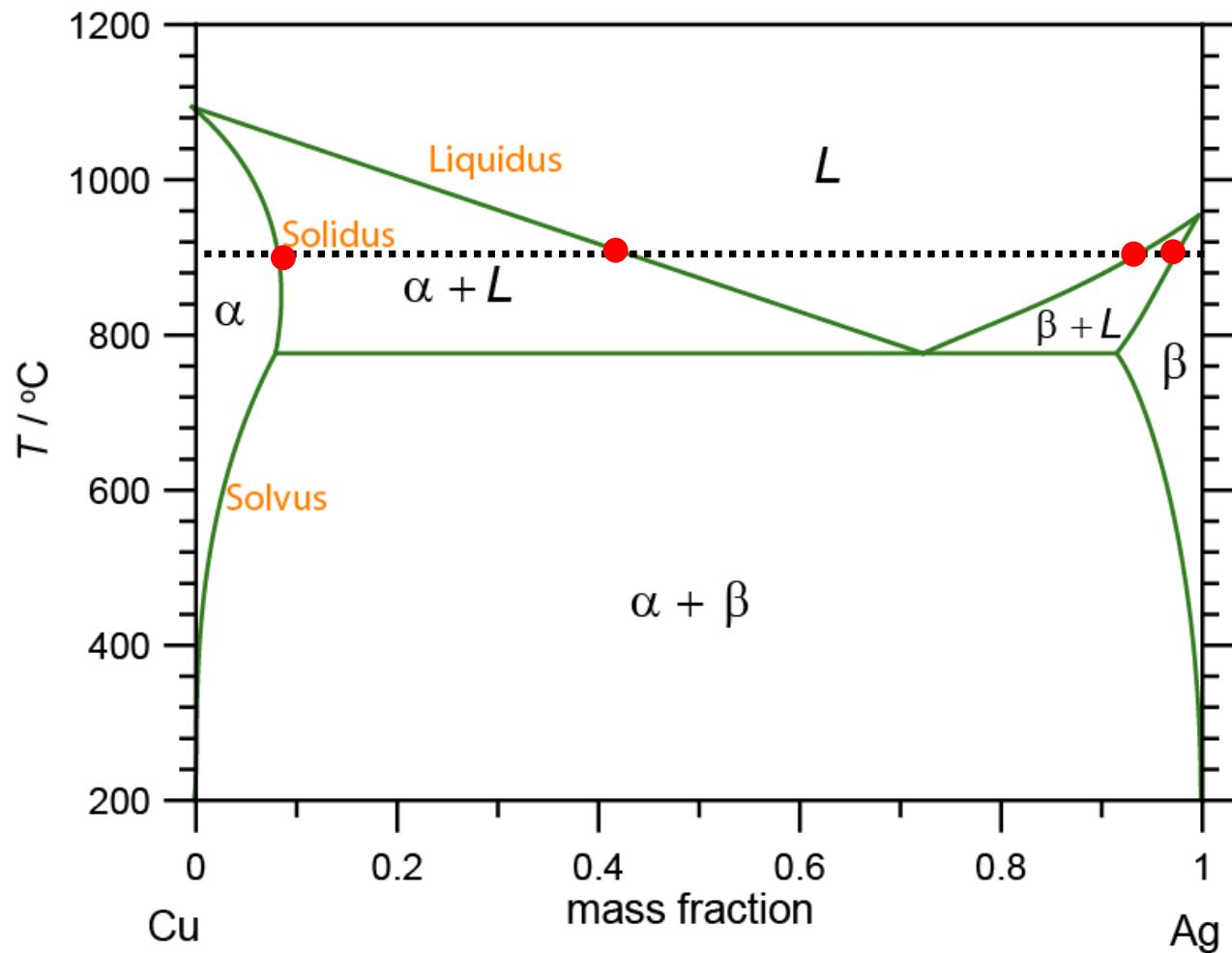
- Eutectisch punt
- oplosbaarheid



Vloeistof-vast-evenwichten

Kenmerken

- Eutectisch punt
- oplosbaarheid



Vloeistof-vast-evenwichten

Kenmerken

- Verbinding
- Eutecticum
- Incongruent smeltpunt

